

A REPORT OF FINDINGS FROM A SHORELINE SURVEY IN THE VICINITY OF  
SEABROOK HARBOR, 1995

And

ASSESSMENT OF THE POTENTIAL FOR FECAL CONTAMINATION OF THE  
SEABROOK CLAMFLATS FROM BOAT DISCHARGE OF WASTES

A Report to

The New Hampshire Office of State Planning  
and

The New Hampshire Division of Public Health Services, Bureau of Food Protection

Submitted by

Dr. Richard Langan and Dr. Stephen H. Jones  
Jackson Estuarine Laboratory, University of New Hampshire

July 19, 1995

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## ACKNOWLEDGEMENTS

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## SUMMARY

A shoreline survey conducted in June of 1995 in the area adjacent to the Seabrook clamflats indicates that seepage of contaminated effluent from riparian properties could potentially impact the growing area. It is recommended that the Seabrook flat remain closed until these residences are connected to the Seabrook municipal sewage treatment plant.

An analysis of dilution/dispersion of contaminants resulting from potential illegal discharge of wastes from boats in Seabrook Harbor indicates that the number and types of vessels present in the harbor during the fall and winter do not pose a risk of contamination of the clamflats. It is recommended, however, that the Seabrook flats remain closed during the time period when pleasure boats and charter fishing vessels are also present in the harbor (mid-May through September).

## INTRODUCTION

A sanitary survey conducted in 1993 and 1994 in the Hampton Harbor Estuary, New Hampshire, resulted in the conditional opening by the NH SSCA (State Shellfish Control Agency; the NH Division of Public Health Services) of the Common Island and Browns River clamflats for recreational harvest. Despite water quality records from the survey period at sites in the vicinity of the Seabrook clamflats or "middle ground", that met conditionally approved classification criteria, the Seabrook flats remained closed due to the close proximity of residences with suspected malfunctioning septic systems and the location of boat moorings in Seabrook Harbor. Results of the continuing sampling program in the fall through spring of 1994-1995 indicated that fecal coliform counts remained low in Seabrook Harbor (east side of Seabrook flats), however several samples in the channel to the West of the Seabrook flats had elevated (>43 FC/100ml) coliform counts. It was suspected that the sources of these intermittent, elevated water scores were septic systems in the vicinity of River Street and/or Cross Beach in Seabrook. Since these sources will be eliminated sometime in the fall/winter of 1995-1996 when the Seabrook Sewage Treatment Plant goes on line, it was determined by the NH CORD Shellfish Committee that it would be important to confirm that these sources of pollution were indeed responsible for the variability in FC counts. The committee agreed that a period of documented improvement in water quality at sample sites

following the start of operation of the Seabrook STP (and hence elimination of the River Street/Cross Beach pollution sources) could result in opening of the Seabrook flats. The one remaining concern was the moored vessels in Seabrook Harbor and the lack of information on dilution and dispersion of contaminants associated with potential unlawful discharge of wastes from the vessels.

Section C 9 of Part I of the National Shellfish Sanitation Program (NSSP 1993) Manual of Operations requires that an analysis of the impact of marinas or mooring areas on adjacent shellfish growing waters be conducted before the area can be properly classified. It was determined by the CORD Shellfish Committee that in addition to revisiting the shoreline adjacent to Seabrook Harbor, that a marina dilution study be conducted as well.

This report describes the results and findings of the shoreline survey work conducted in June 1995 and the modeling of dilution/dispersion of contaminants resulting from vessel discharge of wastes in Seabrook Harbor.

## METHODS

### 1. Shoreline survey in the vicinity of Seabrook Harbor

On June 2, Andrea Tomlinson and Deborah Lamson of the Jackson Estuarine Laboratory conducted a shoreline survey for properties adjacent to Seabrook Harbor. All properties were inspected for the presence of pipes, effluent, suspected malfunctioning septic systems and any other potential sources of pollution to the growing area. Samples for fecal coliform analysis were obtained from those properties with visible effluent and from the adjacent harbor area.

### 2. Dilution/Dispersion modeling of wastes discharged from vessels in Seabrook Harbor

#### A. Information Gathering

The study was initiated by gathering information on: 1) the number and types of vessels moored or docked in Seabrook Harbor; 2) accurate bathymetry and water volumes in the harbor; and 3) circulation of water in the vicinity of the clamflat

1) Vessel information was obtained by researching records on mooring permits at the New Hampshire State Port Authority, examining aerial photographs of the mooring areas in the Harbor, a site visit and photographs of mooring locations and types of vessels, and conversations with the Port Authority Director and the Seabrook Harbor Master.

2) Bathymetry and water volumes were obtained from charts provided by the NH Department of Transportation. The charts resulted from the 1993 dredging of

Seabrook Harbor and provided accurate depths and dimensions of the Harbor. Volumes were calculated using the DOT data and NOAA tidal height data for Hampton Harbor.

3) Data on water circulation and movement was obtained from the current study conducted in June of 1994 as part of the 1993-1994 Sanitary Survey of Hampton harbor. In that study, current speed and direction were measured at two stations in Seabrook Harbor during four intervals each of the ebb and flood tides.

## B. Modeling

Based on the alignment of the moored vessels in the Harbor, the initial thought was that discharge from the vessels could be equated to discharge from a multiport diffuser pipe, and the EPA discharge models MERGE and CORMIX models could be applied to this situation. Since CORMIX is a more robust model than MERGE in terms of predicting plume concentrations in the far field, it was chosen for use in this study. Though many of the assumptions needed to fit the CORMIX model were applicable to this situation, both CORMIX and MERGE are designed for continuous discharge, and therefore not a perfect fit for discharge from moored vessels. In order for the model to fit, it was assumed that all vessels in the area were discharging  $2 \times 10^9$  FC in 12 liters of water over a six hour period. Though this assumption is conservative in that it assumes every vessel is illegally discharging waste in the same six hour period (a highly unlikely scenario) it also assumes that the discharge is slow and continuous, which is also highly unlikely.

In order to better simulate the discharge from a vessel, an advection/dispersion evaluation of a slug injection was used, and the same conservative assumption that each vessel would discharge wastes from one person over a six hour period (however, as a slug discharge) was used. The objectives of the models were to predict the concentration of fecal coliforms in the discharge plume when it comes in contact with the clamflat.

The models were initially run at a worst case scenario; discharge beginning at slack low tide and continuing through the flood tide and treating coliform bacteria as conservative particles. If a discharge occurs during the ebbing tide, except during the slack periods at high or low tides, the longitudinal dispersion due to the ebb tide current velocity carries the plume out of the Seabrook Harbor area without intersecting with the clamflats. Additionally, ebb tide waters flow over the clamflats in a northeasterly direction, resulting in a directional dispersion of any discharge plume from moored vessels away from the clamflats. At slack low tide, however, the incoming water "dead ends" at the southern terminus of Seabrook Harbor until the water is sufficiently high to flow over the clamflat. Vessel discharge of contaminants at this point in time was considered to be the worst case scenario for impact on the clamflats. The initial run of the model assumed a minimum

longitudinal dispersion coefficient (low tidal current velocity of 0.10m/sec), an equal lateral dispersion coefficient (current velocity = 0.1 m/sec) , the least volume dilution low tide, and did not take a decay coefficient (bacterial die-off ) into consideration. A subsequent run of the model used more accurate current velocity and directional vectors as well as conservative decay coefficient for bacterial die-off.

Decay of fecal-borne bacteria in seawater occurs over a wide range of rates, depending on the prevailing environmental conditions. Grazing by bacterivores and sunlight have the most significant impacts on bacterial survival, and rates are decreased ~2x with each 10°C increase in temperature. Solic and Krstulovic (1992) looked at the effects of radiation, temperature, salinity, & pH on fecal coliform survival. They used non-turbid seawater and found no impact on T90 (time for 90% of bacteria to die) at depths to 10 m (T90~5 h). The die-off rate was doubled at 20 vs 10°C. In sunlight at 35 ppt NaCl and ~20°C, they found die-off rate to be 1.02/h. Pommeypuy et al. (1992) measured fecal coliform T90 values of <2 h under high sunlight conditions in the Mediterranean Sea. Sorensen (1991) found *E. coli* to have a half life of ~ 5 h, or 3.3/d, in raw seawater. Valiela et al. (1991) used literature values to estimate fecal coliform death rates in Buttermilk Bay, MA. The high rate of death, based on a T90 of 2.5 h was 22.1/d and the low rate of death, based on a T90 of 15 h was 3.7/d. These values are for death of standing stock fecal coliforms per day, whereas bacteria associated with fresh sewage probably have faster death rates.

A decay rate constant for Hampton Harbor conditions at the marina can be chosen based on the above review of literature values. An estimate of decay constants between 3/d and 20/d seems reasonable, with a compromise, defensible decay rate, of 10/d, or T90 of 5.5 h. This estimate includes consideration of the following assumption:

- bacteria are associated with freshly discharged sewage;
- the bacteria used for the assessment are fecal coliforms;
- discharges occur during daytime when water  $T \geq 10^{\circ}\text{C}$ ;
- receiving water is clear/non-turbid;
- receiving water is near ocean salinity (~35ppt) and low in organic matter;
- effluent medium has no influence on bacterial interaction in water column;
- discharged bacteria remain in water column;
- effluent and bacteria remain in shallow water, <~5 m.



## RESULTS

### 1. Shoreline Survey

Results of the shoreline survey are detailed in Appendix 1. The surveyors found several areas of seepage from suspected malfunctioning septic systems, and several residences with visible pipes that may or may not have been gray water pipes. Though most samples of seep water had very low fecal coliform concentrations, a seep sample collected from a property on the south side of River Street had a fecal coliform concentration of  $\approx 200,000$  FC/100 ml (Table 1, APPENDIX I). This contamination would be transported via the network of tidal creeks through the marsh to the Blackwater River, and potentially impact the Seabrook clamflats during ebb tide. Samples taken from Seabrook Harbor near the Yankee Fisherman's Coop and immediately north of River Street had very low fecal coliform concentrations (Table 1, APPENDIX I).

### 2. Dilution dispersion modeling

#### Input Data

Based on the information obtained from review of mooring permit data, and discussions with the Port Authority Director and the Seabrook Harbormaster, it was determined that there are sixty five mooring permits issued for Seabrook Harbor. No live-aboard vessels are moored or docked in Seabrook Harbor. Vessels are moored more or less in single file running north to south past the coop pier, becoming more dense and clustered immediately south of the pier. Approximately 50% of the moorings are issued to pleasure craft in the 15'-26' LOA. These vessels, in addition to the Eastman charter fishing fleet, occupy the harbor seasonally (May through September). The remaining moorings are occupied by commercial fishing vessels which consist of small draggers, gillnetters and lobster boats, most of which are < 50' LOA. From mid-October through mid-May, approximately 35 commercial fishing vessels remain moored in Seabrook Harbor, as the pleasure craft and charter vessels are hauled out for the season. The commercial vessels are for the most part, day fishing boats that leave the harbor between 3-4 AM, fish the nearshore (generally <10 miles from shore) waters of the Gulf of Maine and return to unload their catch at the Cooperative in the early afternoon. For the purpose of both the CORMIX model and the slug discharge evaluation, it was assumed that each of the 35 vessels discharged wastes from one person over a six hour period.

The moorings begin approximately 100 meters north of the Yankee Fisherman's Cooperative and extends southward past the Coop pier and bulkhead ( $\approx 100$  m wide) for approximately 300 meters southward to the terminus of the

harbor channel at the Seabrook town pier and launch ramp and the Eastman Fishing Fleet pier and docks on River Street. The estimated total length of the mooring area is 500 m. At the northern end of the mooring area, the channel is 61 m wide, increasing to 77 m in width at the center of the Coop pier. South of the pier, the channel width increases to 101 m. Based on channel width and mooring density, an average width of 96 m and an average length of 300 m were used in the CORMIX model and slug discharge evaluation and assuming that vessels are moored in approximately mid-channel, the distance to the clamflat was estimated to be 48 m (Fig. 1).

The depth throughout the channel is approximately 3 m at MLW (Figs 2 and 3). The tidal prism in the harbor is 2.6 m, nearly doubling the harbor volume at MHW. Flood tide water will begin to flow over the clamflat when water level has risen approximately 0.61 m, or approximately 2.0 hrs. past the time of MLW. At hour 2.0, the average current velocity in the harbor channel is approximately 0.3 m/sec flowing due south (NH DPHS 1994). Lateral velocity of incoming water over the clamflat, perpendicular to the direction of the flood waters in the channel was estimated at 0.10 cm/sec. The initial run of the CORMIX model and the slug discharge evaluation used a longitudinal velocity of 0.10 and an equal lateral velocity (Appendix II). In order to more accurately simulate hydrographic conditions at the time that flood tide water contacts the clamflats, a subsequent run of CORMIX and the slug discharge evaluation used 0.30 m/sec longitudinal velocity and 0.10 m/sec for a lateral velocity and a decay coefficient of 10/day (Appendix III).

Results of the initial run of CORMIX are detailed in Appendix II A. Results of the run indicated that the concentration of the plume at the time of its intersection with the clamflat is 17.2 CFU/100 ml, which exceeds the allowable limit of 14 FC/100ml (Appendix II (page 2)). When the slug injection evaluation (Appendix II B) was run using the initial parameters and no decay coefficient, the concentration of the plume at the time of intersection with the clamflat was 30.0 CFU/100ml (Appendix II (page 3)).

Subsequent runs of the CORMIX model and the slug discharge evaluation used a the decay coefficient described in the Methods section of this report, a longitudinal velocity of 0.30 m/sec, and a lateral velocity of 0.10 m/sec. Using these input data, CORMIX estimated that the concentration of the plume is 0.0176 FC/100 ml (Appendix III (pg A-2)) while the slug injection evaluation estimated that the plume concentration is 13 FC/100 ml when it intersects the clamflat. Both estimates are below the regulatory limit of 14 FC/100 ml.

## DISCUSSION

Based on the findings of the shoreline survey update for the Seabrook Harbor area, it appears that residences adjacent to the harbor area should continue to be considered potential pollution sources which may impact the sanitary quality of the growing waters. The residences of concern are located on Cross Beach Road and the south side of River Street, adjacent to the marsh that connects with the Blackwater River via a network of small tidal creeks. Impact to the water in the river was not observed, however, the presence of contaminated seep water adjacent to the marsh was confirmed. Several Cross Beach residences on stilts had what appeared to be discharge pipes coming out of the bottom of the houses directed toward the ground. Though no discharge was observed, the presence of these pipes is suspect.

Though routine monitoring indicates that the water quality is for the most part within the regulatory limit of 14 FC/100 ml, water samples taken near these residences indicate that contaminated effluent may intermittently affect the growing area. It is recommended that the Seabrook clamflat should remain closed until these residences are connected to the Seabrook Municipal Sewage Treatment Plant.

Guidance for control of areas used as a marina provided by Part I of the NSSP manual (NSSP 1993) requires that water circulation, water volume and mixing rate, as well as consideration of the number and types of vessels in an area be evaluated when considering the closure zone adjacent to a marina. Based on the analysis conducted for this report, the vessels that are present in the harbor from mid-October to mid-May do not pose a risk of contamination of the Seabrook clamflats at a level that would require closing the area. If the recreational vessels that occupy the moorings and docks (including the Eastman fleet) at the peak of the boating season (mid-May through September) are included in the analysis, there would be potential risk of contamination of the growing area from illegal discharge of wastes. It is recommended therefore that the flats remain closed from mid-May through September, or until the pleasure craft and charter vessels are removed for the season.

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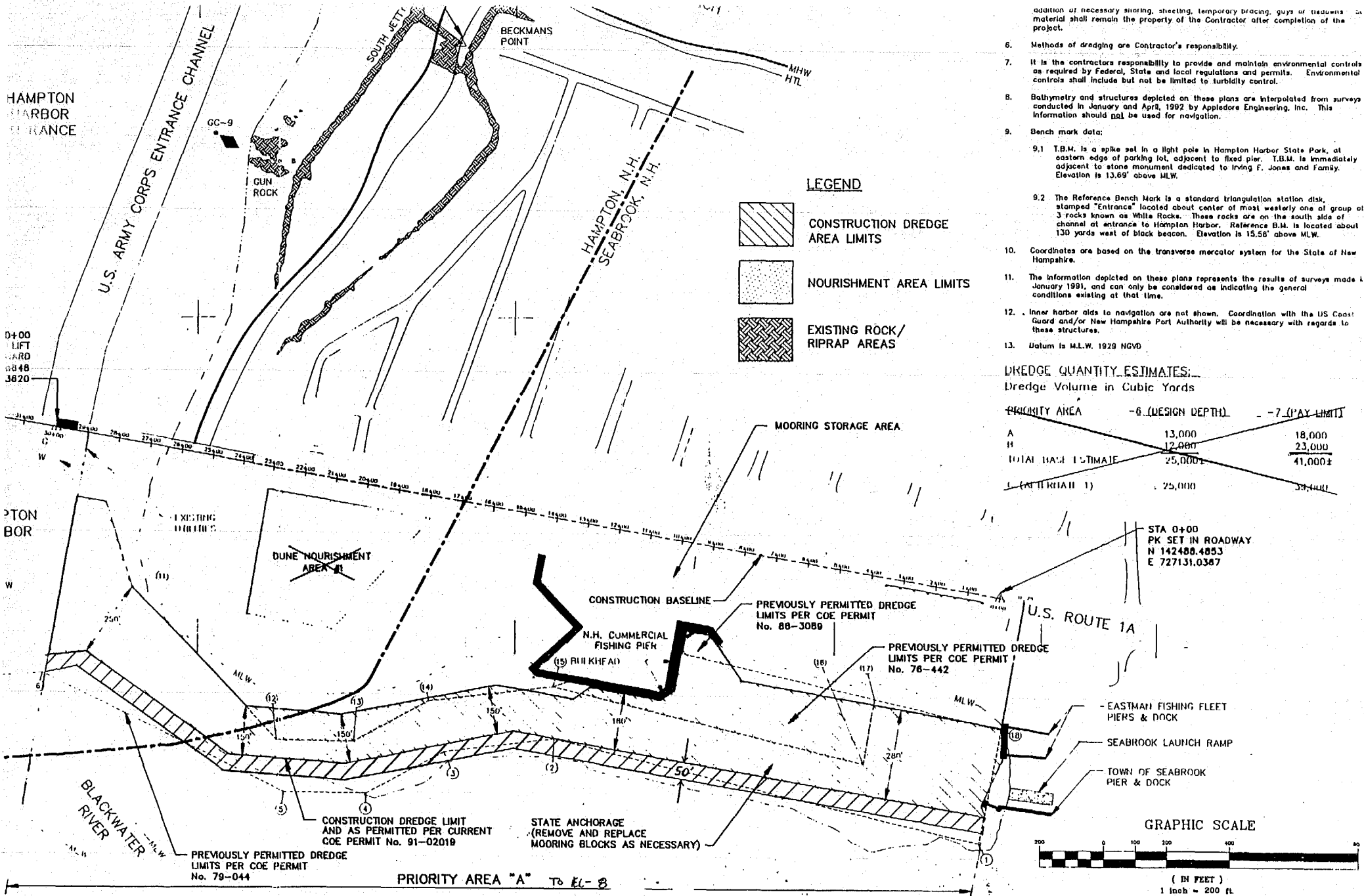


Figure 1. Schematic of Seabrook Harbor showing shape and dimensions of the harbor

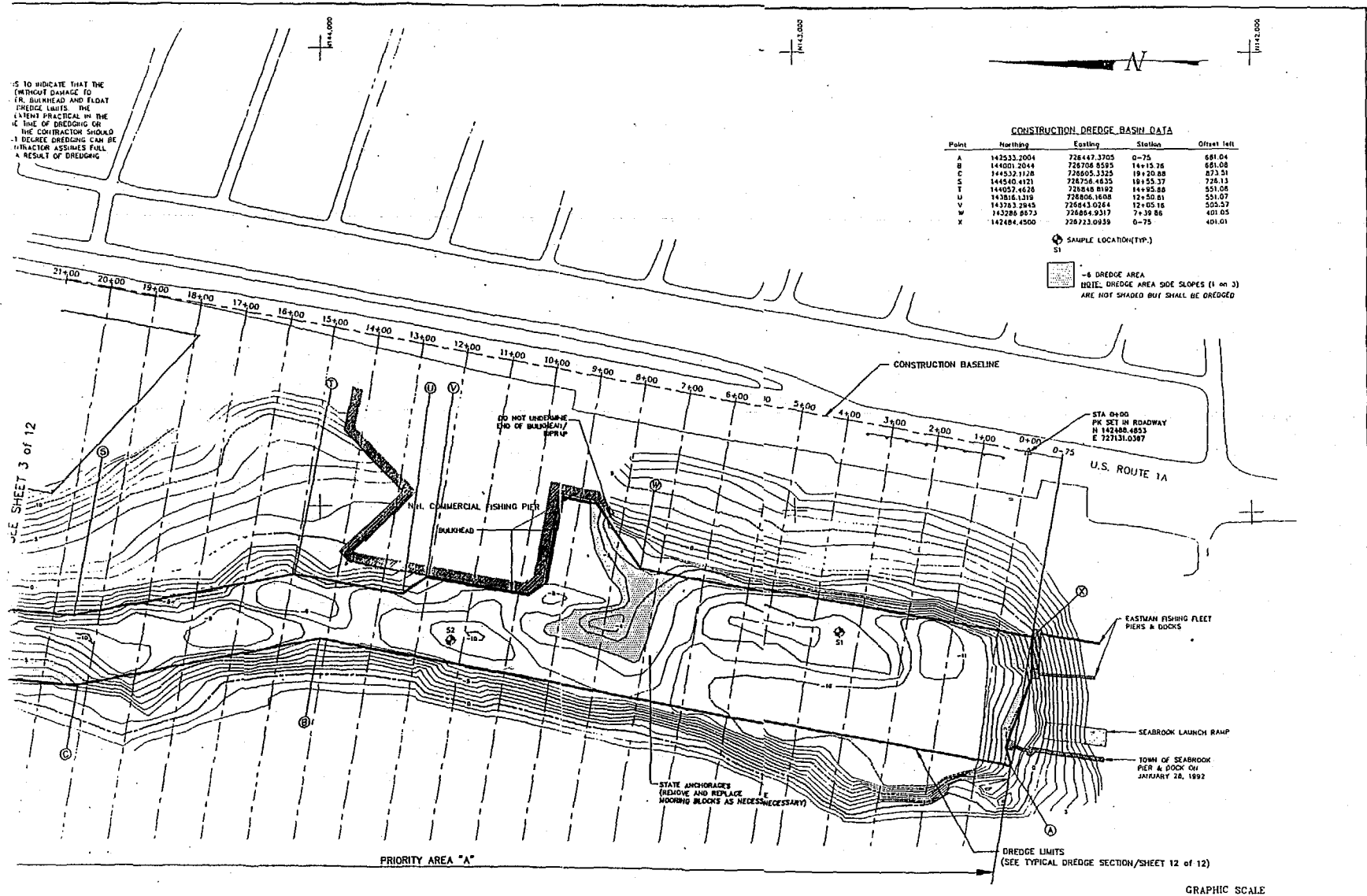


Figure 2. Schematic of Seabrook Harbor showing depth contours and dredge areas

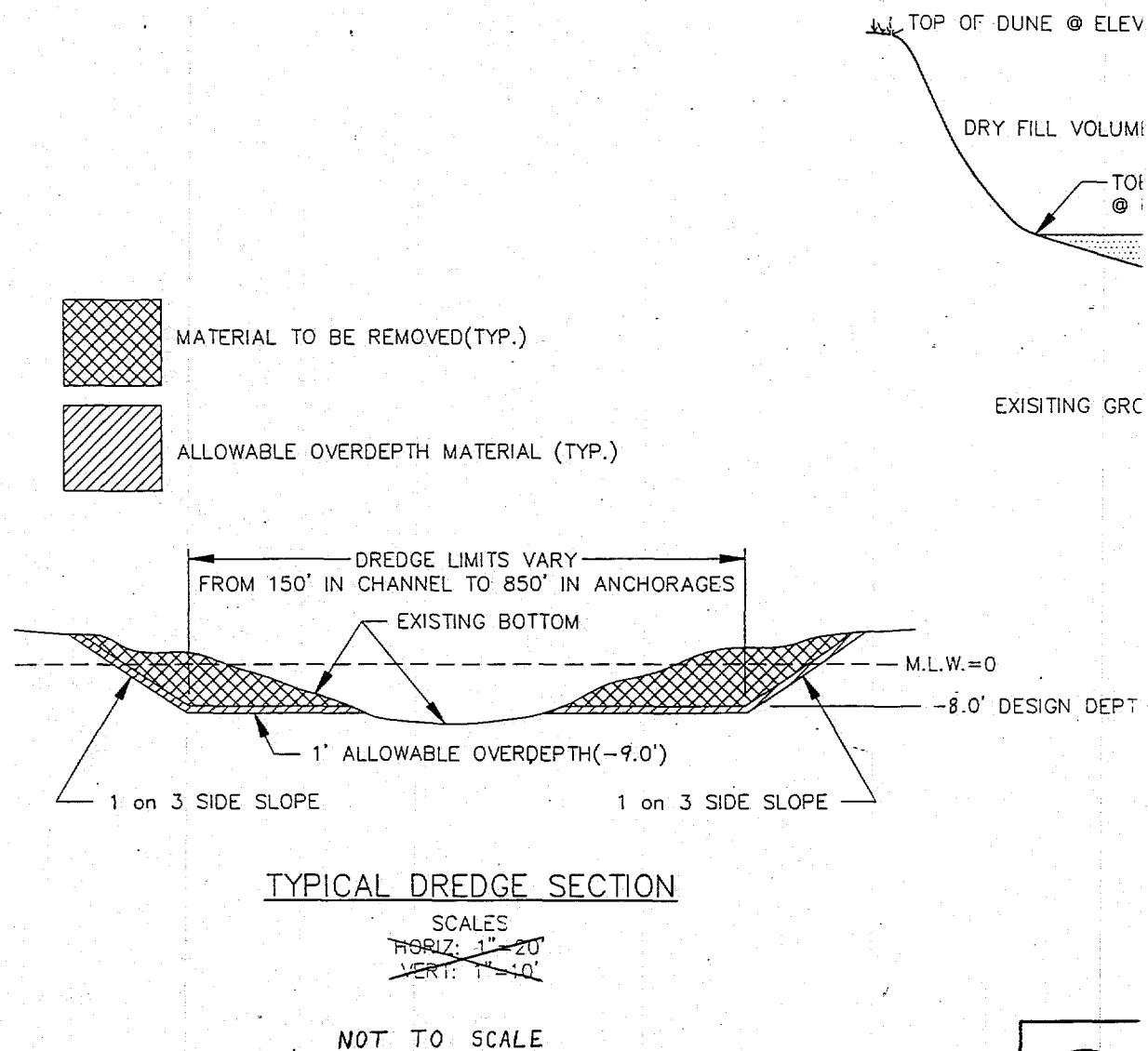


Figure 3. Cross section of the Seabrook Harbor channel showing depth and slope of dredged area

## **APPENDIX I**

### **Seabrook Harbor Shoreline Survey**



## Seabrook Harbor Shoreline Survey Field Report Summary

Friday, 6/2/95

The surveyors present were Andrea Tomlinson and Deborah Lamson. After crossing the Route 1A bridge into Seabrook, we parked at the public beach parking lot (first lot on the right) to inspect the Yankee Fisherman's Coop and the surrounding shoreline. The Seabrook Public Works crew was pumping groundwater out at the roadside and draining it into the harbor. This was done the previous week throughout the area in preparation for the new sewer lines which are being installed in the Seabrook. Groundwater from the canvas pipes which were draining into the harbor at the rock wall next to the coop were sampled. Results of sample analyses are presented in Table 1.

At River Street, we began the shoreline inspection along the harbor at Eastman's. At the Hopkinson/Pike/Camacho properties there is a large granite retaining wall on the shore. From under the wall seepage was draining directly into the harbor over an area of >60 feet in length. Two samples were taken at each end of the seepage along with two samples of the harbor water just offshore from the seepage site.

On the south side of River Street facing the marsh, other suspected pollution sources were found. At the Welch residence, a 3" PVC pipe was discharging gray water into the abutting marshland. A water sample of the discharge was obtained. Next to this pipe, coming from under the wooden backyard fence was a small pool of dark-colored, foul smelling water. Next to the Welch residence were the Knowles. A sample was taken from a stagnant tidal pool which appeared to originate from the backyard via a drainage stream underneath the backyard fence. Further down the road, going back toward Rt. 1A and Eastman's, we discovered a black-colored stream of water coming from underneath a wood pile about four feet in height between the Gynan and Kent residence. The origin appeared to be coming from the Kent property, as there was evidence (dirt heaped up in a straight line) of an underground pipe which led in the direction of their home. A sample of this seepage was obtained.

From River Street, we went to Cross Beach Road where we saw that all twenty trailer and homes had newly installed manholes for the new sewer lines. At the end of the road, we found numerous wooden houses on stilts with black or white (PVC) piping coming from the center of the houses and draining onto the ground directly underneath the houses. These pipes were possibly gray water pipes, though no active discharges were observed. All twenty trailers/homes are situated on hydric marshland/dunes and it is suspected that most if not all have unsuitable septic and graywater treatment. Small livestock were observed at one of the residences on the south side of Cross Beach Road. Among the animals visible were three goats and seven ducks.

**Table 1. Seabrook Harbor Shoreline Survey**

**River St. and Cross Beach Rd., Seabrook, NH: Fecal coliform levels.**

House #	Location	Description	Owner	Map #	FC/100ml
14	14 River St.	Seepage-1	Hopkinson	SB 1	<5
14	14 River St.	Seepage-2	Hopkinson	SB 1	<5
30	30 River St.	Gray water pipe	Welch	SB 1	Bkgd *
31	31 River St.	Septic seepage	Knowles	SB 1	60
36/37	Between 36 & 37 River St.	Septic seepage	Gynan/Kent	SB 1	~200000
NA	Harbor at River St.	Harbor sample	NA	SB 1	0
NA	Rocks at Yankee Coop	Groundwater	Town of Seabrook	SB 1	1

\* Bkgd- Background growth interference extensive; couldn't read

## **APPENDIX II**

### **Initial Runs of CORMIX Model and Slug Injection Evaluation**

Diffusion Study on  
Contamination of the Seabrook Clamflat  
in Hampton Harbor

Holly E. Clark

Report Prepared for:

Dr. Richard Langan  
June 20, 1995

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Fluids Lab Graduate Office  
Department of Civil Engineering  
Kingsbury Hall  
Durham, NH 03824

June 20, 1995

Dr. Richard Langan  
Jackson Estuarine Laboratory  
Durham, NH 03824

Subject: Diffusion Study on Contamination of the Seabrook Clamflat in Hampton Harbor

Dear Dr. Langan:

The southeastern region of Hampton Harbor, located in Seabrook, NH, was evaluated using CORMIX, a diffuser modeling program. The diffusion of discharges from moored vessels in the channel was investigated. The purpose was to estimate the concentrations of fecal coliform that would appear in the clamflat adjacent to the channel.

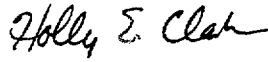
The result of the study shows that the high concentration associated with the vessel discharge would not be reduced to safe levels before it reaches the clamflat. The CORMIX modeling assumed that the discharge would be released over a period of 6 hours. The result of the diffuser model shows that the fecal coliform count remains at 17.2 CFU/100mL as it flows over the clamflat. This is above the acceptable limit of 14 CFU/100mL.

The CORMIX model shows the result of the release from the vessel as if it were mixed slowly with the tidewater. The release from a vessel would occur as a slug rather than a continuous release rationed out over time. Therefore, the CORMIX model is not appropriate for this application. Through the use of an advection-dispersion model, the dilution of the discharge from a vessel is found to be somewhat less. The resulting concentration to reach the mudflat could be approximately 30 CFU/100mL.

Due to the high concentration of  $2 \times 10^9$  CFU in a 12L vessel release, it is not likely that adequate mixing and dispersion could occur within the channel reaches and prevent contamination of the clamflat. A tracer study using a slug injection method at a mooring in the harbor could be used to demonstrate the spreading and movement of the vessel discharge into the area of interest. It is likely that the tracer study would support the conclusion that the contamination would occur.

The details of the study are included in the report. Thank you for considering me for this study. Please feel free to call at 862-3623 if you have any questions or comments.

Sincerely,

  
Holly E. Clark

## I. Introduction:

### Description of Area

This study concerns the southeastern region of Hampton Harbor that is located in Seabrook, NH. A channel along the eastern shore of the harbor is approximately 96m (315 ft) wide by 500m (1640 ft) long by 3m (10 ft) deep at low tide. A mudflat flanks the west bank of the channel. During the flood of the tide cycle, the channel fills with water, overflows across the mudflat, and fills the harbor. During the ebb, the mudflat drains to the West and the channel drains to the North. There are moorings located along the centerline of the channel that are approximately 48m (158 ft) east of the mudflat.

### Assumptions for Modeling

The purpose of this study is to investigate the possibility that the clam beds in the mudflats (clamflats) will be contaminated by discharges from the moored boats. This study is based on modeling the diffusion of the discharge into the flow of the water through this area. The program used to model this situation is not designed for this application. Adjustments were made to the "actual" situation to fit the model parameters. The assumptions used in the modeling are as follows:

- There are 35 equally spaced vessels moored 300m (984 ft) along the centerline of the channel;
- Each vessel discharges once over a 6 hr period;
- Each discharge is 12 L (3.2gal) with a fecal coliform count of  $2 \times 10^9$  CFU per discharge;
- The effluent is assumed to be dispensed continuously for 6 hrs;
- Due to the short duration, no decay coefficient is used;
- The density of the effluent is  $1010.15 \text{ kg/m}^3$ ;
- The channel is 3m (9.8 ft) deep relative to the mudflat;
- The tide flows south in the channel for 2 hrs, then flows west over the mudflat for 4 hrs;
- The velocity in the channel and over the mudflat is 0.1m/s (0.2 knots);
- The effluent over the mudflat is discharged from 35 ports;
- The initial concentration of the effluent over the mudflat is determined from the plume in the channel.

## II. Modeling Studies:

### CORMIX Modeling

The CORMIX modeling program models the effluent discharged from a diffuser in a stream. It is used to determine the concentration gradient in the plume. In this case a multiport diffuser placed along the centerline of the channel simulates the moored vessels. The discharge of the vessels was converted to a flow rate over a half tide cycle of 6 hours. The assumption is that if all the vessels discharge in that period of time, the worst case will be investigated.

The CORMIX model was run in two stages. The first stage assumed that the initial vessel discharge was occurring as the channel was filling. A mass balance equation was used to determine the initial concentration in the effluent if 0.1 m/s (0.33 ft/s) velocity and 0.051m (2 in) diameter ports were used. The resulting concentration was 5426700 CFU/100mL (Appendix A). The first stage determined that the discharge from the diffuser is fully mixed vertically and laterally in the channel in approximately 2 hours. The concentration of the mixture is 5380 CFU/100mL as shown in the CORMIX output (Appendix A). The total colony forming units (CFU) discharged by the 35 vessels was used in a mass balance equation to determine the flow rate at the new concentration to be discharged over the clamflat in a 4 hour period. The resulting flow rate of 0.1m<sup>3</sup>/s (3.5cfs) was used to determine the size of the discharge ports. The diameter of the ports at 0.18m (7.1 in) maintained the 0.1 m/s (0.33 ft/s) discharge velocity (Appendix A).

The second stage of the CORMIX model was run for a 500m (1640 ft) wide stream that was 1m (3.3 ft) deep. The diffuser had 35 ports and was centered in the channel perpendicular to the westerly flow of the incoming tide. The model predicted that the concentration would remain at 17.2 CFU/100mL as it flowed over the clamflat (Appendix A). A second model with the clamflat "stream" at 1.5m (4.9 ft) deep found the concentration stabilizing at 11.9 CFU/100mL



(Appendix A). Although the depth over the clamflat ranges from 0 to 2.5m (0 to 8.2 ft), an average constant depth of either the 1m (3.3 ft) or 1.5m (4.9 ft) was used to run the model.

There are many differences between the model and the actual situation. The CORMIX model assumes steady flow with a continuous discharge in a small stream. The tide is flowing into the channel so the depth is constantly increasing which is unsteady flow. Each vessel is “actually” discharging an entire 12 L (3.2 gal) slug into the channel. The injections from 35 vessels are intermittent. The channel is similar to a stream as it fills but the flow “backs up” rather than flowing downstream. The flow of the water changes direction as the water rises enough to flow over the mudflat. The vessels are discharging near the surface and the model assumes a diffuser is positioned near the bottom.

The model simulation is less conservative than the actual conditions because of these differences. The most important disparity is the adjustment from intermittent injections to a continuous discharge. The model is seeing a discharge that is already spread out over time. It is assumed that the continuous injection would show a continuous plume that is similar in dimensions to a single moving plume from a slug injection. From there, the second stage of modeling was performed.

#### Advection-Dispersion Evaluation of a Slug Injection

A second way of looking at this situation is to use an advection-dispersion equation for a slug injection. The McQuivey and Keefer equation for the dispersion coefficient was used. The assumptions for this modeling are:

- Bed slope is 0.001;
- Stream is 96m (315 ft) wide by 3m (9.8 ft) deep;
- Velocity of the seawater is constant at 0.1 m/s (0.2 knots).

The dispersion coefficient was determined to be 17.4 (Appendix B). The discharge from one vessel was assumed to be fully mixed at 360m (1181 ft) downstream. The concentration was determined to be 1.93 CFU/100mL when fully mixed in a 96m (315 ft) wide by 3m (9.8 ft) deep by 360m (1181 ft) long section of the channel. Using the dispersion coefficient in an advection-dispersion equation resulted in a peak concentration of 1.4 CFU/100mL at 360m (1181 ft) downstream. The dispersion coefficient appears to be appropriate. This method was applied to the discharge from a vessel flowing directly at the mudflat during a tidal flow velocity of 0.1m/s (0.2 knots). The result shows that a peak concentration of approximately 30 CFU/100mL will reach the mudflat (Appendix B). This is above the acceptable limit of 14 CFU/100mL.

#### Mass Balance

Another way of viewing the situation is based on mass balances. The discharge from one vessel is assumed to be fully mixed in a hypothetical cylindrical volume centered on the vessel. The concentration throughout this cylinder is 14 CFU/100mL. Using a mass balance equation, when the channel is 3m (9.8 ft) deep the radius of the cylinder is 39m (128 ft). This shows that if the water is stagnant and mixing is complete (somehow), the discharge from a vessel could be diffused prior to reaching the mudflats. Adding in a velocity for the tidal water of 0.1m/s (0.2 knots) results in the fully mixed hypothetical cylinder reaching the mudflat in 1.5 minutes. The effluent does not mix in this manner but it does illustrate the likelihood that the fecal coliform concentration would not be reduced sufficiently before reaching the mudflats.

### **III. Conclusion:**

Although the CORMIX method used is not fully applicable to the situation, the predictions tend to show that the clamflats could see concentrations above the maximum level of 14 CFU/mL. The use of the advection-dispersion equation on a single vessel discharge also shows that the clamflats could be contaminated by the discharge.

The velocity of the water in the channel moves the effluent quickly over the relatively short distance from the moorings to the clamflat. The high concentration of the effluent requires a large volume of water to reduce it to 14 CFU/100mL. If the assumptions concerning the effluent concentration and channel characteristics are correct, it is apparent that a single vessel discharge into the channel might not mix adequately with the ambient water to achieve 14 CFU/100mL within 48m (158 ft) of the mooring.

A tracer study using a slug injection method into the harbor could be used to demonstrate the advection and dispersion of the vessel discharge into the area of interest. It is likely that the tracer study would support the conclusion that there is inadequate mixing of the vessel discharge.

## Appendix A



Given:

35 vessels

Discharge per vessel = 12 L

One discharge per vessel over 6 hrs.

Initial concentration is  $2 \times 10^9$  CFU/12 L

Find:

Concentration of effluent if it is discharged through 35 ports of 0.051 m diameter each at a velocity of 0.1 m/s.

① finding total discharge of vessels,  $Q_T$

$$Q_T = \frac{(35 \text{ vessels})(12 \text{ L})(0.001 \text{ m}^3/\text{L})}{6 \text{ hr} (3600 \text{ sec/hr})} = 1.944 \times 10^{-5} \text{ m}^3/\text{s}$$

② finding area of 35 ports,  $A$

$$A = \frac{(0.051)^2 \pi (35)}{4} = 0.0715 \text{ m}^2$$

③ finding discharge from multiport diffuser,  $Q_D$

$$Q_D = VA = (0.1 \text{ m/s})(0.0715 \text{ m}^2) = 0.00715 \text{ m}^3/\text{s}$$

④ finding concentration of discharge from multiport diffuser,  $C_D$

$$\frac{Q_T C_i}{Q_D} = C_D = \frac{(1.94 \times 10^{-5} \text{ m}^3/\text{s})(2 \times 10^9 \text{ CFU}/100 \text{ mL})}{0.00715 \text{ m}^3/\text{s}} = \underline{\underline{5426700 \text{ CFU}/100 \text{ mL}}}$$

Stage 1: Assume effluent is discharged from a multiport

diffuser with 35 ports. The ports alternate on the diffuser pipe. Port diameter is 0.051 m.

Spacing of the ports is 3.3 m on a 300 m long diffuser. The pipe is positioned along the centerline of the channel in a North-South direction.

This effluent flow rate assumes that all the vessels are discharging slowly for 6 hrs simultaneously.

## CHECKLIST FOR DATA PREPARATION

A2

## CORMIX -- CORNELL MIXING ZONE EXPERT SYSTEM -- CORMIX

SITE Name Seabrook Harbor Mudflat Date: 6/17  
 Design CASE Multipoint discharge into channel Prepared by: H2Cleb  
 DOS FILE NAME Staeelma (w/o extension)

AMBIENT DATA: Water body is bounded/unbounded  
 Water body depth 3 m If bounded: Width 96 m  
 Depth at discharge 3 m Appearance (1)2/3  
 Ambient flowrate        m<sup>3</sup>/s or: Ambient velocity 0.1 m/s  
 Manning's n 0.014 or: Darcy-Weisbach f (0.010)  
 Wind speed 2 m/s  
 Density data: UNITS: Density...kg/m<sup>3</sup> / Temperature...°C  
 Water body is fresh/salt water If fresh: Specify as density/temp. values  
 If uniform: Average density/temp. 1010.5  
 If stratified: Density/temp. at surface         
 Stratification type A/B/C Density/temp. at bottom         
 If B/C: Pycnocline height        m If C: Density/temp. jump       

DISCHARGE DATA: Specify geometry for CORMIX1 or 2 or 3

## SUBMERGED SINGLE PORT DISCHARGE -- CORMIX1

Nearest bank is on left/right Distance to nearest bank        m  
 Vertical angle THETA        ° Horizontal angle SIGMA        °  
 Port diameter        m or: Port area        m<sup>2</sup>  
 Port height        m

## SUBMERGED MULTIPOINT DIFFUSER DISCHARGE -- CORMIX2

Nearest bank is on left/right Distance to one endpoint 48 m  
 Diffuser length 300 m to other endpoint 48 m  
 Total number of openings 35  
 Port diameter 0.051 m with contraction ratio K = 1  
 Diffuser arrangement/type unidirectional / staged / alternating or vertical (B), (A)  
 Alignment angle GAMMA 0 ° Horizontal angle SIGMA        °  
 Vertical angle THETA 40 ° Relative orientation BETA        °  
 Port height 0.99 m (A) = holes (single ports)

## BUOYANT SURFACE DISCHARGE -- CORMIX3

Discharge located on left/right bank Configuration flush/protruding/co-flowing  
 Horizontal angle SIGMA        ° If protruding: Dist. frm bank        m  
 Depth at discharge        m Bottom slope        °  
 If rectangular Width        m or: If circular Diameter        m  
 discharge channel: Depth        m pipe: Bottom invert depth        m

Effluent: Flow rate 0.00714 m<sup>3</sup>/s or: Effluent velocity (0.1) m/s  
 Effluent density 1010.15 kg/m<sup>3</sup> or: Effluent temperature        °C  
 Heated discharge? yes/no If yes: Heat loss coefficient        W/m<sup>2</sup>, °C  
 Concentration units CFU-Per-100mL Effluent concentration 5426700  
 Conservative substance? yes/no If no: Decay coefficient        /day

## MIXING ZONE DATA:

Is effluent toxic? yes/no If yes: CMC value 14  
 CCC value 14  
 WQ stand./conventional poll.? yes/no If yes: value of standard         
 Any mixing zone specified? yes/no If yes: distance        m  
 or width        % or m  
 or area        % or m<sup>2</sup>  
 Region of interest 1000 m

# CORNELL MIXING ZONE EXPERT SYSTEM

Submerged Multiport Diffuser Discharges CMX2 v.2.10

May 1993

```
Site name/label:      Seabrook^Harbor^Mudflat
Design case:          Multiport^discharge^at^300m^
FILE NAME:            cormix\sim\stagelma.cx2
Time of Fortran run:  06/17/95--10:33:01
```

### Bounded section

```

BS      =      96.00  AS      =      288.00  QA      =      28.80
HA      =       3.00  HD      =       3.00
UA      =       .100  F       =       .011  USTAR = .3651E-02
UW      =      2.000  UWSTAR= .2198E-02
Uniform density environment
STRCND=  U          RHOAM = 1010.5000

```

## DITYPE=alternating parallel

BETYPE=alternating without fanning

BANK	=	LEFT	DISTB	=	.00	YB1	=	48.00	YB2	=	48.00
LD	=	300.00	NOPEN	=	35	SPAC	=	8.82			
D0	=	.051	A0	=	.002	H0	=	.99			
GAMMA	=	.00	THETA	=	90.00						
SIGMA	=	.00	BETA	=	90.00						
U0	=	.100	Q0	=	.007						
RH00	=	1010.1500	DRH00	=	.3500E+00	GP0	=	.3396E-02			
C0	=	.5427E+07	CUNITS	=	CFU-per-100mL						
IPOLL	=	1	KS	=	.0000E+00	KD	=	.0000E+00			

The bank/shore proximity effect is accounted for by the following flow variables and definitions of length scales and parameters.

$$LD = 300.00 \quad Q0 = .014 \quad (Q0 = .1428E-01)$$

```
q0      = .9500E-04  m0      = .2370E-05  j0      = .8067E-07  SIGNJ0=      1.0
```

Associated 2-d length scales (meters)

```
1Q=B      =      .001 1M      =      .13 1m      =      .00
1mp      = 99999.00 1bp      = 99999.00 1a      = 99999.00
```

QO = .1428E-01 MO = .7111E-03 JO = .2420E-04

Associated 3-d length scales (meters)

LQ	=	.41	LM	=	.89	Lm	=	.35	Lb	=	.05
						Lmp	=	99999.00	Lbp	=	99999.00

```
FR0      =      110.99  FRD0 =      7.58  R      =      .99
(slot)      (port/nozzle)
```

222

2	Flow class (CORMIX2)	=	MU1H	2
2	Applicable layer depth HS	=	3.00	2





---

 BEGIN MOD243: DENSITY CURRENT DEVELOPING ALONG PARALLEL DIFFUSER LINE

The plume for this parallel diffuser interacts with the surface/pycnocline or the bottom, and a DENSITY CURRENT forms.

Note: The starting x-coordinate of the developing plume will be shifted upstream.

Profile definitions:

BV = top-hat thickness, measured vertically

BH = top-hat half-width, measured horizontally in y-direction

ZU = upper plume boundary (Z-coordinate)

ZL = lower plume boundary (Z-coordinate)

S = hydrodynamic average (bulk) dilution

C = average (bulk) concentration (includes reaction effects, if any)

X	Y	Z	S	C	BV	BH
323.04	.00	3.00	2834.8	.191E+04	.90	.90
383.04	.00	3.00	4009.0	.135E+04	3.00	.96
443.04	.00	3.00	4009.0	.135E+04	3.00	1.01
503.04	.00	3.00	4009.0	.135E+04	3.00	1.07
563.04	.00	3.00	4009.0	.135E+04	3.00	1.13
623.04	.00	3.00	4009.0	.135E+04	3.00	1.19

Cumulative travel time = 7730. sec

---

 END OF MOD243: DENSITY CURRENT DEVELOPING ALONG PARALLEL DIFFUSER LINE

---

 \*\* End of NEAR-FIELD REGION (NFR) \*\*

Recall that the plume is symmetric to the bank/shore on which the centerline (X-axis) is located.

The LIMITING DILUTION (given by ambient flow/discharge ratio) is: 1009.4

This value is below the computed dilution of 4009.0 at the end of the NFR.

Mixing for this discharge configuration is constrained by the ambient flow.

The previous module predictions are unreliable since the limiting dilution cannot be exceeded for this diffuser in deep unstratified layer.

A subsequent module (MOD281) will predict the properties of the cross-sectionally fully mixed plume with limiting dilution and will compute a POSSIBLE UPSTREAM WEDGE INTRUSION.

---

 BEGIN MOD281: MIXED PLUME/BOUNDED CHANNEL/POSSIBLE UPSTREAM WEDGE INTRUSION

The DOWNSTREAM flow field for this unstable shallow water discharge is VERTICALLY FULLY MIXED.

The mixing is controlled by the limiting dilution = 1009.4 ←

Channel DENSIMETRIC FROUDE NUMBER (FCHAN) for this mixed flow = 31.47

No upstream wedge intrusion takes place since FCHAN exceeds the critical value of 0.7.

X	Y	Z	S	C	BV	BH	ZU	ZL
623.04	.00	3.00	1009.4	.538E+04	3.00	96.00	3.00	.00

Cumulative travel time = 7730. sec = 2.15 hr

VERTICALLY AND Laterally FULLY MIXED over layer depth: END OF SIMULATION!

[illegible]

## CORMIX SESSION REPORT:

XX

## CORMIX: CORNELL MIXING ZONE EXPERT SYSTEM

CORMIX v.2.10

May 1993

SITE NAME/LABEL: Seabrook Harbor Mudflat  
 DESIGN CASE: Multiport discharge at 300m  
 FILE NAME: stagelma  
 Using subsystem CORMIX2: Submerged Multiport Diffuser Discharges  
 Start of session: 06/17/95--10:26:52

\*\*\*\*\*

## SUMMARY OF INPUT DATA:

-----  
AMBIENT PARAMETERS:

Cross-section	=	bounded
Width	BS	= 96 m
Channel regularity	=	1
Ambient flowrate	QA	= 28.80 m <sup>3</sup> /s
Average depth	HA	= 3 m
Depth at discharge	HD	= 3 m
Ambient velocity	UA	= .1 m/s
Darcy-Weisbach friction factor	F	= 0.0106
Calculated from Manning's n	=	.014
Wind velocity	UW	= 2 m/s
Stratification Type	STRCND	= U
Surface density	RHOAS	= 1010.5 kg/m <sup>3</sup>
Bottom density	RHOAB	= 1010.5 kg/m <sup>3</sup>

-----  
DISCHARGE PARAMETERS:

## Submerged Multiport Diffuser Discharge

Diffuser type	DITYPE	=	alternating parallel
Diffuser length	LD	=	300 m
Nearest bank	=	left	
Diffuser endpoints	YB1	=	48 m; YB2 = 48 m
Number of openings	NOPEN	=	35
Spacing between risers/openings	SPAC	=	8.82 m
Port/Nozzle diameter	D0	=	.051 m
Equivalent slot width	B0	=	0.0002 m
Total area of openings	A0	=	0.0020 m <sup>2</sup>
Discharge velocity	U0	=	0.09 m/s
Total discharge	Q0	=	.00714 m <sup>3</sup> /s
Discharge port height	H0	=	.99 m
Nozzle arrangement	BETTYPE	=	alternating without fanning
Diffuser alignment angle	GAMMA	=	0 deg
Vertical discharge angle	THETA	=	90.0 deg
Horizontal discharge angle	SIGMA	=	0.0 deg
Relative orientation angle	BETA	=	90.0 deg
Discharge density	RHO0	=	1010.15 kg/m <sup>3</sup>
Density difference	DRHO	=	0.3500 kg/m <sup>3</sup>
Buoyant acceleration	GP0	=	.0034 m/s <sup>2</sup>
Discharge concentration	C0	=	5426700 CFU-per-100mL
Surface heat exchange coeff.	KS	=	0 m/s
Coefficient of decay	KD	=	0 /s

-----  
FLUX VARIABLES PER UNIT DIFFUSER LENGTH:

Discharge (volume flux)	q0	=	0.000095 m <sup>2</sup> /s
Momentum flux	m0	=	0.000004 m <sup>3</sup> /s <sup>2</sup>
Buoyancy flux	j0	=	0 m <sup>3</sup> /s <sup>3</sup>

-----  
DISCHARGE/ENVIRONMENT LENGTH SCALES :

lq =	0.00 m	lm =	0.00 m	lM =	0.12 m
------	--------	------	--------	------	--------

1m' = 99999.0 m      1b' = 99999.0 m      1a = 99999.0 m  
(These refer to the actual discharge/environment length scales.)

#### NON-DIMENSIONAL PARAMETERS:

Slot Froude number	FR0	=	110.99
Port/nozzle Froude number	FRD0	=	7.58
Velocity ratio	R	=	0.99

#### MIXING ZONE / TOXIC DILUTION ZONE / AREA OF INTEREST PARAMETERS:

Toxic discharge		=	yes
CMC concentration	CMC	=	14 CFU-per-100mL
CCC concentration	CCC	=	14 CFU-per-100mL
Water quality standard		=	given by CCC value
Regulatory mixing zone		=	no
Region of interest		=	1000.00 m downstream

\*\*\*\*\*

#### HYDRODYNAMIC CLASSIFICATION:

\*-----\*

FLOW CLASS	=	MU1H	
------------	---	------	--

\*-----\*

This flow configuration applies to a layer corresponding to the full water depth at the discharge site.

Applicable layer depth = water depth = 3 m

\*\*\*\*\*

#### MIXING ZONE EVALUATION (hydrodynamic and regulatory summary):

#### X-Y-Z Coordinate system:

Origin is located at the bottom below the port center:  
0.0 m from the left bank/shore.

#### NEAR-FIELD REGION (NFR) CONDITIONS :

Note: The NFR is the zone of strong initial mixing. It has no regulatory implication. However, this information may be useful for the discharge designer because the mixing in the NFR is usually sensitive to the discharge design conditions.

Pollutant concentration at edge of NFR	=	1353.6320 CFU-per-100mL
Dilution at edge of NFR	=	4008.9 ← This dilution is not possible as seen in the prediction file:
NFR Location:	x =	623.04 m
(centerline coordinates)	y =	.00 m
	z =	3.00 m
NFR plume dimensions:	half-width =	1.18 m
	thickness =	3.00 m

#### Buoyancy assessment:

The effluent density is less than the surrounding ambient water density at the discharge level.

Therefore, the effluent is POSITIVELY BUOYANT and will tend to rise towards the surface.

#### \*\*\*\*\* TOXIC DILUTION ZONE SUMMARY \*\*\*\*\*

Criterion maximum concentration (CMC)	=	14 CFU-per-100mL
Corresponding dilution	=	.0

The CMC value was not encountered within the specified simulation distance.

Plume dilution values are too low to meet CMC.

#### \*\*\*\*\* REGULATORY MIXING ZONE SUMMARY \*\*\*\*\*

No RMZ has been specified.

The CCC for the toxic pollutant was not encountered within the predicted plume region.

#### \*\*\*\*\* FINAL DESIGN ADVICE AND COMMENTS \*\*\*\*\*

CORMIX2 uses the TWO-DIMENSIONAL SLOT DIFFUSER CONCEPT to represent

In the present design, the spacing between adjacent ports/nozzles (or riser assemblies) is of the order of, or less than, the local water depth so that the slot diffuser approximation holds well. Nevertheless, if this is a final design, the user is advised to use a final CORMIX1 (single port discharge) analysis, with discharge data for an individual diffuser jet/plume, in order to compare to the present near-field prediction.

DIFFUSER DESIGN DETAILS: Because of the alternating arrangement of the opposing nozzles/ports, the AVERAGE VERTICAL ANGLE (THETA) has been set to 90 deg. This represents a ZERO NET HORIZONTAL MOMENTUM FLUX for the entire diffuser.

This parallel diffuser lies in CLOSE PROXIMITY to the bank (shoreline). The shoreline will act as a REFLECTING BOUNDARY for the flow field. This effect has been represented by doubling all flow variables.

REMINDER: The user must take note that HYDRODYNAMIC MODELING by any known technique is NOT AN EXACT SCIENCE.

Extensive comparison with field and laboratory data has shown that the CORMIX predictions on dilutions and concentrations (with associated plume geometries) are reliable for the majority of cases and are accurate to within about  $\pm 50\%$  (standard deviation).

As a further safeguard, CORMIX will not give predictions whenever it judges the design configuration as highly complex and uncertain for prediction.

\*\*\*\*\*

```
DESIGN CASE: Multiport discharge at 300m
FILE NAME: stagelma
Subsystem CORMIX2: Submerged Multiport Diffuser Discharges
END OF SESSION/ITERATION: 06/30/95--08:57:11
```

[illegible]



The Department of Civil Engineering  
College of Engineering and Physical Sciences  
The University of New Hampshire  
Kingsbury Hall  
33 College Road  
Durham, New Hampshire 03824-3591

Project/Problem Set:

Cormix Modeling

Detail/Problem:

Stage 2 -

Class:

Prof:

Sheet: A10 of 25

Calc. by: Holly Clark

Date: 6/17/95

Chck. by:

Date:

Stage 2: Assume effluent is discharged from a multiport diffuser with 35 ports. The diffuser pipe is positioned along the center line of the channel with all the ports facing the same direction. The discharge from the ports is co-flowing with the water toward the mudflat. The "stream" is 500 m wide flowing west. Two simulations were run, once at a depth of 1 m and once at 1.5 m. The initial concentration of the effluent was the value taken as the fully mixed concentration from Stage 1. The density was assumed to match ambient.

Given:  $2 \times 10^9$  CFU per vessel  
35 Vessels  
Initial concentration = 5380 CFU/100 mL

Find: Port diameter for 35 equal sized ports if discharge is continuous for 4 hrs. at a velocity of 0.1 m/s.

① finding volume,  $V$

$$V = \frac{(2 \times 10^9 \text{ CFU})(35)}{5380 \text{ CFU}/100 \text{ mL}} (1 \times 10^{-6} \text{ m}^3/\text{mL}) = 1301 \text{ m}^3$$

② finding total discharge,  $Q$

$$Q = 1301 \text{ m}^3 / 4 \text{ hr} (3600 \text{ s/hr}) = 0.0903 \text{ m}^3/\text{s}$$

③ finding area of Port,  $A$

$$A = \frac{Q}{V} = \frac{0.0903 \text{ m}^3/\text{s}}{0.1 (35)} = 0.0259 \text{ m}^2/\text{port}$$

④ finding diameter of Port,  $d$

$$d = \sqrt{\frac{4A}{\pi}} = 0.18 \text{ m}$$

# CORMIX -- CORNELL MIXING ZONE EXPERT SYSTEM -- CORMIX

SITE Name Brook Harbor Mudflat Date: 6/17/95  
 Design CASE multiport discharge over mudflat Prepared by: #5 CLO  
 DOS FILE NAME Stage 2.m (w/o extension)

**AMBIENT DATA:**  
 Water body is bounded/unbounded  
 Water body depth 1 m If bounded: Width 500 m  
 Depth at discharge 1 m Appearance (1/2/3)  
 Ambient flowrate 0.014 m<sup>3</sup>/s or: Ambient velocity 0.1 m/s  
 Manning's n 0.014 or: Darcy-Weisbach f (0.015)  
 Wind speed 2 m/s  
**Density data:** UNITS: Density...kg/m<sup>3</sup> / Temperature...°C  
 Water body is fresh/salt water If fresh: Specify as density/temp. values  
 If uniform: Average density/temp. 1010.5  
 If stratified: Density/temp. at surface \_\_\_\_\_  
 Stratification type A/B/C Density/temp. at bottom \_\_\_\_\_  
 If B/C: Pycnocline height \_\_\_\_\_ m If C: Density/temp. jump \_\_\_\_\_

**DISCHARGE DATA:** Specify geometry for CORMIX1 or 2 or 3

## SUBMERGED SINGLE PORT DISCHARGE -- CORMIX1

Nearest bank is on left/right Distance to nearest bank \_\_\_\_\_ m  
 Vertical angle THETA \_\_\_\_\_ ° Horizontal angle SIGMA \_\_\_\_\_ °  
 Port diameter \_\_\_\_\_ m or: Port area \_\_\_\_\_ m<sup>2</sup>  
 Port height \_\_\_\_\_ m

## SUBMERGED MULTIPOINT DIFFUSER DISCHARGE -- CORMIX2

Nearest bank is on left/right Distance to one endpoint 100 m  
 Diffuser length 300 m to other endpoint 400 m  
 Total number of openings 35  
 Port diameter 0.18 m with contraction ratio 1  
 Diffuser arrangement/type unidirectional/staged / alternating or vertical A single port  
 Alignment angle GAMMA 90 ° Horizontal angle SIGMA 0 °  
 Vertical angle THETA 0 ° Relative orientation BETA 90 °  
 Port height .33 m A unidirectional & staged diffuser

## BUOYANT SURFACE DISCHARGE -- CORMIX3

Discharge located on left/right bank Configuration flush/protruding/co-flowing  
 Horizontal angle SIGMA \_\_\_\_\_ ° If protruding: Dist. frm bank \_\_\_\_\_ m  
 Depth at discharge \_\_\_\_\_ m Bottom slope \_\_\_\_\_ °  
 If rectangular Width \_\_\_\_\_ m or: If circular Diameter \_\_\_\_\_ m  
 discharge channel: Depth \_\_\_\_\_ m pipe: Bottom invert depth \_\_\_\_\_ m

Effluent: Flow rate 0.1 m<sup>3</sup>/s or: Effluent velocity (0.11) m/s  
 Effluent density 1010.5 kg/m<sup>3</sup> or: Effluent temperature \_\_\_\_\_ °C  
 Heated discharge? yes/no If yes: Heat loss coefficient \_\_\_\_\_ W/m<sup>2</sup>,°C  
 Concentration units CFU-per-100mL Effluent concentration 5380  
 Conservative substance? yes/no If no: Decay coefficient \_\_\_\_\_ /day

## MIXING ZONE DATA:

Is effluent toxic? yes/no If yes: CMC value 14  
 CCC value 14  
 WQ stand./conventional poll.? yes/no If yes: value of standard \_\_\_\_\_  
 Any mixing zone specified? yes/no If yes: distance \_\_\_\_\_ m  
 or width \_\_\_\_\_ % or m  
 or area \_\_\_\_\_ % or m<sup>2</sup>  
 Region of interest 5000 m  
 Grid intervals for display 6

[illegible]

## Subsystem version:

May 1993

```
Site name/label:      Seabrook^Harbor^Mudflat
Design case:          Multiport^discharge^over^mudflat
FILE NAME:            cormix\sim\stage2m .cx2
Time of Fortran run:  06/17/95--11:54:30
```

```

BS      =      500.00  AS      =      500.00  QA      =      50.00
HA      =      1.00   HD      =      1.00
UA      =      .100   F       =      .015  USTAR = .4384E-02
UW      =      2.000  UWSTAR= .2198E-02
Uniform density environment
STRCND=  U           RHOAM = 1010.5000

```

BANK	=	LEFT	DISTB	=	250.00	YB1	=	100.00	YB2	=	400.00
LD	=	300.00	NOPEN	=	35	SPAC	=	8.82			
D0	=	.180	A0	=	.025	H0	=	.33			
GAMMA	=	90.00	THETA	=	.00						
SIGMA	=	.00	BETA	=	90.00						
U0	=	.112	Q0	=	.100						
RH00	=	1010.5000	DRH00	=	.0000E+00	GP0	=	.0000E+00			
C0	=	.5380E+04	CUNITS	=	CFU-per-100mL						
IPOLL	=	1	KS	=	.0000E+00	KD	=	.0000E+00			

```

q0      = .3330E-03  m0      = .3738E-04  j0      = .0000E+00  SIGNJ0=      1.0
Associated 2-d length scales (meters)
lQ=B    =      .003  lM      = 99999.00  lm      =      .00
lmp     = 99999.00  lbp     = 99999.00  la      = 99999.00

```

LQ	=	.95	LM	=	99999.00	Lm	=	1.05	Lb	=	.00
						Lmp	=	99999.00	Lbp	=	99999.00

```
FR0    = 99999.00   FRD0 = 99999.00   R      =      1.12
(slot)                (port/nozzle)
```

[illegible]

C0 = .5380E+04 CUNITS= CFU-per-100mL



NTOX = 1                      CMC = .1400E+02    CCC = CSTD  
 NSTD = 1                      CSTD = .1400E+02  
 REGMZ = 0  
 XINT = 5000.00    XMAX = 5000.00

(1m)

# X-Y-Z COORDINATE SYSTEM:

ORIGIN is located at the bottom and the diffuser mid-point:  
 250.00 m from the LEFT bank/shore.

X-axis points downstream, Y-axis points to left, Z-axis points upward.

NSTEP = 6 display intervals per module

## BEGIN MOD201: DIFFUSER DISCHARGE MODULE

### Profile definitions:

BV = Gaussian 1/e (37%) half-width, in vertical plane normal to trajectory

BH = top-hat half-width, in horizontal plane normal to trajectory

S = hydrodynamic centerline dilution

C = centerline concentration (includes reaction effects, if any)

X	Y	Z	S	C	BV	BH
.00	.00	.33	1.0	.538E+04	.00	150.00

## END OF MOD201: DIFFUSER DISCHARGE MODULE

## BEGIN MOD271: ACCELERATION ZONE OF UNIDIRECTIONAL CO-FLOWING DIFFUSER

In this laterally contracting zone the diffuser plume becomes VERTICALLY FULLY MIXED over the entire layer depth (HS = 1.00m).

Full mixing is achieved after a plume distance of about five layer depths from the diffuser.

### Profile definitions:

BV = layer depth (vertically mixed)

BH = top-hat half-width, in horizontal plane normal to trajectory

S = hydrodynamic average (bulk) dilution

C = average (bulk) concentration (includes reaction effects, if any)

X	Y	Z	S	C	BV	BH
.00	.00	1.00	1.0	.538E+04	1.00	150.00
25.00	.00	1.00	302.3	.178E+02	1.00	149.89
50.00	.00	1.00	302.3	.178E+02	1.00	149.82
75.00	.00	1.00	302.3	.178E+02	1.00	149.77
100.00	.00	1.00	302.3	.178E+02	1.00	149.74
125.00	.00	1.00	302.3	.178E+02	1.00	149.73
150.00	.00	1.00	302.3	.178E+02	1.00	149.72

Cumulative travel time = 1494. sec

## END OF MOD271: ACCELERATION ZONE OF UNIDIRECTIONAL CO-FLOWING DIFFUSER

## BEGIN MOD251: DIFFUSER PLUME IN CO-FLOW

Phase 1: Vertically mixed, Phase 2: Re-stratified

Phase 1: The diffuser plume is VERTICALLY FULLY MIXED over the entire layer depth.

This flow region is INSIGNIFICANT in spatial extent and will be by-passed.



## CORMIX SESSION REPORT:

XX

## CORMIX: CORNELL MIXING ZONE EXPERT SYSTEM

CORMIX v.2.10

May 1993

SITE NAME/LABEL: Seabrook Harbor Mudflat  
 DESIGN CASE: Multiport discharge over mudflat  
 FILE NAME: stage2m  
 Using subsystem CORMIX2: Submerged Multiport Diffuser Discharges  
 Start of session: 06/17/95--11:34:05

\*\*\*\*\*

## SUMMARY OF INPUT DATA:

## AMBIENT PARAMETERS:

Cross-section		=	bounded
Width	BS	=	500 m
Channel regularity		=	1
Ambient flowrate	QA	=	50 m <sup>3</sup> /s
Average depth	HA	=	1 m
Depth at discharge	HD	=	1 m
Ambient velocity	UA	=	.1 m/s
Darcy-Weisbach friction factor	F	=	0.0153
Calculated from Manning's n		=	.014
Wind velocity	UW	=	2 m/s
Stratification Type	STRCND	=	U
Surface density	RHOAS	=	1010.5 kg/m <sup>3</sup>
Bottom density	RHOAB	=	1010.5 kg/m <sup>3</sup>

## DISCHARGE PARAMETERS:

## Submerged Multiport Diffuser Discharge

Diffuser type	DITYPE	=	unidirectional perpendicular
Diffuser length	LD	=	300 m
Nearest bank		=	left
Diffuser endpoints	YB1	=	100 m; YB2 = 400 m
Number of openings	NOPEN	=	35
Spacing between risers/openings	SPAC	=	8.82 m
Port/Nozzle diameter	D0	=	.18 m
Equivalent slot width	B0	=	0.0029 m
Total area of openings	A0	=	0.0254 m <sup>2</sup>
Discharge velocity	U0	=	0.11 m/s
Total discharge	Q0	=	.1 m <sup>3</sup> /s
Discharge port height	H0	=	.33 m
Nozzle arrangement	BETTYPE	=	unidirectional without fanning
Diffuser alignment angle	GAMMA	=	90 deg
Vertical discharge angle	THETA	=	0 deg
Horizontal discharge angle	SIGMA	=	0 deg
Relative orientation angle	BETA	=	90 deg
Discharge density	RHO0	=	1010.5 kg/m <sup>3</sup>
Density difference	DRHO	=	0 kg/m <sup>3</sup>
Buoyant acceleration	GP0	=	.0000 m/s <sup>2</sup>
Discharge concentration	C0	=	5380 CFU-per-100mL
Surface heat exchange coeff.	KS	=	0 m/s
Coefficient of decay	KD	=	0 /s

## FLUX VARIABLES PER UNIT DIFFUSER LENGTH:

Discharge (volume flux)	q0	=	0.000333 m <sup>2</sup> /s
Momentum flux	m0	=	0.000037 m <sup>3</sup> /s <sup>2</sup>
Buoyancy flux	j0	=	0 m <sup>3</sup> /s <sup>3</sup>

## DISCHARGE/ENVIRONMENT LENGTH SCALES :

lq =	0.00 m	lm =	0.00 m	1M =	99999.0 m
------	--------	------	--------	------	-----------

1m' = 99999.0 m      1b' = 99999.0 m      1a = 99999.0 m  
 (These refer to the actual discharge/environment length scales.)

#### NON-DIMENSIONAL PARAMETERS:

Slot Froude number	FR0	=	99999.0
Port/nozzle Froude number	FRD0	=	99999.0
Velocity ratio	R	=	1.12

#### MIXING ZONE / TOXIC DILUTION ZONE / AREA OF INTEREST PARAMETERS:

Toxic discharge		=	yes
CMC concentration	CMC	=	14 CFU-per-100mL
CCC concentration	CCC	=	14 CFU-per-100mL
Water quality standard		=	given by CCC value
Regulatory mixing zone		=	no
Region of interest		=	5000.00 m downstream

\*\*\*\*\*

#### HYDRODYNAMIC CLASSIFICATION:

\*-----\*  
 | FLOW CLASS = MU2 |  
 \*-----\*

This flow configuration applies to a layer corresponding to the full water depth at the discharge site.

Applicable layer depth = water depth = 1 m

\*\*\*\*\*

#### MIXING ZONE EVALUATION (hydrodynamic and regulatory summary):

#### X-Y-Z Coordinate system:

Origin is located at the bottom below the port center:  
 250 m from the left bank/shore.

#### NEAR-FIELD REGION (NFR) CONDITIONS :

Note: The NFR is the zone of strong initial mixing. It has no regulatory implication. However, this information may be useful for the discharge designer because the mixing in the NFR is usually sensitive to the discharge design conditions.

Pollutant concentration at edge of NFR		=	17.7957 CFU-per-100mL
Dilution at edge of NFR		=	302.3
NFR Location:	x	=	150.00 m
(centerline coordinates)	y	=	.00 m
	z	=	1.00 m
NFR plume dimensions:	half-width	=	149.72 m
	thickness	=	1.00 m

#### Buoyancy assessment:

The effluent density is equal or about equal to the surrounding ambient water density at the discharge level.

Therefore, the effluent behaves essentially as NEUTRALLY BUOYANT.

#### Near-field instability behavior:

The diffuser flow will experience instabilities with full vertical mixing in the near-field.

There may be benthic impact of high pollutant concentrations.

#### FAR-FIELD MIXING SUMMARY:

Plume becomes vertically fully mixed at 150.00 m downstream.

\*\*\*\*\* TOXIC DILUTION ZONE SUMMARY \*\*\*\*\*

Criterion maximum concentration (CMC)	=	14 CFU-per-100mL
Corresponding dilution	=	.0

The CMC value was not encountered within the specified simulation distance.

Plume dilution values are too low to meet CMC.

\*\*\*\*\* REGULATORY MIXING ZONE SUMMARY \*\*\*\*\*

No RMZ has been specified.

The CCC for the toxic pollutant was not encountered within the predicted plume region.

\*\*\*\*\* FINAL DESIGN ADVICE AND COMMENTS \*\*\*\*\*

CORMIX2 uses the TWO-DIMENSIONAL SLOT DIFFUSER CONCEPT to represent the actual three-dimensional diffuser geometry. Thus, it approximates the details of the merging process of the individual jets from each port/nozzle.

In the present design, the spacing between adjacent ports/nozzles (or riser assemblies) is somewhat greater (in the range between three times to ten times) the local water depth. It is unlikely that sufficient lateral interaction of adjacent jets will occur in the near-field. However, the individual jets/plumes may merge soon after in the intermediate-field or in the far-field.

CORMIX2 may have LIMITED APPLICABILITY for this discharge situation.

The results may be somewhat unrealistic in the near-field (minimum dilution may be overpredicted), but appear to be applicable for the intermediate- and far-field processes.

The user is advised to use a subsequent CORMIX1 (single port discharge) analysis, using discharge data for an individual diffuser jet/plume, in order to compare to the present near-field prediction.

REMINDER: The user must take note that HYDRODYNAMIC MODELING by any known technique is NOT AN EXACT SCIENCE.

Extensive comparison with field and laboratory data has shown that the CORMIX predictions on dilutions and concentrations (with associated plume geometries) are reliable for the majority of cases and are accurate to within about  $\pm 50\%$  (standard deviation).

As a further safeguard, CORMIX will not give predictions whenever it judges the design configuration as highly complex and uncertain for prediction.

\*\*\*\*\*

DESIGN CASE: Multiport discharge over mudflat

FILE NAME: stage2m

Subsystem CORMIX2: Submerged Multiport Diffuser Discharges

END OF SESSION/ITERATION: 06/30/95--09:01:00

[illegible]



NTOX = 1 CMC = .1400E+02 CCC = CSTD  
 NSTD = 1 CSTD = .1400E+02  
 REGMZ = 0  
 XINT = 5000.00 XMAX = 5000.00

X-Y-Z COORDINATE SYSTEM:

ORIGIN is located at the bottom and the diffuser mid-point:  
 250.00 m from the LEFT bank/shore.

X-axis points downstream, Y-axis points to left, Z-axis points upward.

NSTEP = 6 display intervals per module

BEGIN MOD201: DIFFUSER DISCHARGE MODULE

Profile definitions:

BV = Gaussian 1/e (37%) half-width, in vertical plane normal to trajectory  
 BH = top-hat half-width, in horizontal plane normal to trajectory  
 S = hydrodynamic centerline dilution  
 C = centerline concentration (includes reaction effects, if any)

X	Y	Z	S	C	BV	BH
.00	.00	.33	1.0	.538E+04	.00	150.00

END OF MOD201: DIFFUSER DISCHARGE MODULE

BEGIN MOD271: ACCELERATION ZONE OF UNIDIRECTIONAL CO-FLOWING DIFFUSER

In this laterally contracting zone the diffuser plume becomes VERTICALLY FULLY MIXED over the entire layer depth (HS = 1.50m).

Full mixing is achieved after a plume distance of about five layer depths from the diffuser.

Profile definitions:

BV = layer depth (vertically mixed)  
 BH = top-hat half-width, in horizontal plane normal to trajectory  
 S = hydrodynamic average (bulk) dilution  
 C = average (bulk) concentration (includes reaction effects, if any)

X	Y	Z	S	C	BV	BH
.00	.00	1.50	1.0	.538E+04	1.50	150.00

\*\* CMC HAS BEEN FOUND \*\*

The pollutant concentration in the plume falls below CMC value of .140E+02 in the current prediction interval.

This is the extent of the TOXIC DILUTION ZONE.

\*\* WATER QUALITY STANDARD OR CCC HAS BEEN FOUND \*\*

The pollutant concentration in the plume falls below water quality standard or CCC value of .140E+02 in the current prediction interval.

This is the spatial extent of concentrations exceeding the water quality standard or CCC value.

25.00	.00	1.50	453.2	.119E+02	1.50	149.93
50.00	.00	1.50	453.2	.119E+02	1.50	149.88
75.00	.00	1.50	453.2	.119E+02	1.50	149.85
100.00	.00	1.50	453.2	.119E+02	1.50	149.83
125.00	.00	1.50	453.2	.119E+02	1.50	149.82
150.00	.00	1.50	453.2	.119E+02	1.50	149.82

Cumulative travel time = 1496. sec

END OF MOD271: ACCELERATION ZONE OF UNIDIRECTIONAL CO-FLOWING DIFFUSER

-----  
BEGIN MOD251: DIFFUSER PLUME IN CO-FLOW

Phase 1: Vertically mixed, Phase 2: Re-stratified

Phase 1: The diffuser plume is VERTICALLY FULLY MIXED over the  
entire layer depth.

This flow region is INSIGNIFICANT in spatial extent and will be by-passed.

-----  
Phase 2: The flow has RESTRATIFIED at the beginning of this zone.

This flow region is INSIGNIFICANT in spatial extent and will be by-passed.

END OF MOD251: DIFFUSER PLUME IN CO-FLOW

-----  
\*\* End of NEAR-FIELD REGION (NFR) \*\*

-----  
BEGIN MOD241: BUOYANT AMBIENT SPREADING

Discharge is non-buoyant or weakly buoyant.

Therefore BUOYANT SPREADING REGIME is ABSENT.

END OF MOD241: BUOYANT AMBIENT SPREADING

-----  
BEGIN MOD261: PASSIVE AMBIENT MIXING IN UNIFORM AMBIENT

Vertical diffusivity (initial value) = .129E-02 m<sup>2</sup>/s

Horizontal diffusivity (initial value) = .161E-02 m<sup>2</sup>/s

The passive diffusion plume is VERTICALLY FULLY MIXED at beginning of region.

Profile definitions:

BV = Gaussian s.d.\*sqrt(pi/2) (46%) thickness, measured vertically  
= or equal to layer depth, if fully mixed

BH = Gaussian s.d.\*sqrt(pi/2) (46%) half-width,  
measured horizontally in Y-direction

ZU = upper plume boundary (Z-coordinate)

ZL = lower plume boundary (Z-coordinate)

S = hydrodynamic centerline dilution

C = centerline concentration (includes reaction effects, if any)

Plume Stage 1 (not bank attached):

X	Y	Z	S	C	BV	BH	ZU	ZL
150.00	.00	1.50	453.2	.119E+02	1.50	151.07	1.50	.00
958.33	.00	1.50	453.6	.119E+02	1.50	151.20	1.50	.00
1766.67	.00	1.50	454.0	.118E+02	1.50	151.34	1.50	.00
2575.00	.00	1.50	454.4	.118E+02	1.50	151.47	1.50	.00
3383.33	.00	1.50	454.8	.118E+02	1.50	151.61	1.50	.00
4191.67	.00	1.50	455.2	.118E+02	1.50	151.74	1.50	.00
5000.00	.00	1.50	455.6	.118E+02	1.50	151.88	1.50	.00

Cumulative travel time = 49996. sec

Simulation limit based on maximum specified distance = 5000.00 m.

This is the REGION OF INTEREST limitation.

-----  
END OF MOD261: PASSIVE AMBIENT MIXING IN UNIFORM AMBIENT

-----  
Because of the fairly LARGE SPACING between adjacent risers/nozzles/ports,





## CORMIX SESSION REPORT:

XX

## CORMIX: CORNELL MIXING ZONE EXPERT SYSTEM

CORMIX v.2.10

May 1993

SITE NAME/LABEL: Seabrook Harbor Mudflat  
 DESIGN CASE: Multiport discharge over one and a half m  
 FILE NAME: stage2mb  
 Using subsystem CORMIX2: Submerged Multiport Diffuser Discharges  
 Start of session: 06/17/95--11:59:22

\*\*\*\*\*

## SUMMARY OF INPUT DATA:

-----  
AMBIENT PARAMETERS:

Cross-section		=	bounded
Width	BS	=	500 m
Channel regularity		=	1
Ambient flowrate	QA	=	75 m <sup>3</sup> /s
Average depth	HA	=	1.5 m
Depth at discharge	HD	=	1.5 m
Ambient velocity	UA	=	.1 m/s
Darcy-Weisbach friction factor	F	=	0.0134
Calculated from Manning's n		=	.014
Wind velocity	UW	=	2 m/s
Stratification Type	STRCND	=	U
Surface density	RHOAS	=	1010.5 kg/m <sup>3</sup>
Bottom density	RHOAB	=	1010.5 kg/m <sup>3</sup>

-----  
DISCHARGE PARAMETERS:

Diffuser type	DITYPE	=	Submerged Multiport Diffuser Discharge
Diffuser length	LD	=	unidirectional perpendicular
Nearest bank		=	300 m
Diffuser endpoints	YB1	=	left
Number of openings	NOPEN	=	100 m; YB2 = 400 m
Spacing between risers/openings	SPAC	=	35
Port/Nozzle diameter	DO	=	8.82 m
Equivalent slot width	BO	=	.18 m
Total area of openings	AO	=	0.0029 m
Discharge velocity	UO	=	0.0254 m <sup>2</sup>
Total discharge	QO	=	0.11 m/s
Discharge port height	HO	=	.1 m <sup>3</sup> /s
Nozzle arrangement	BETYPE	=	.33 m
Diffuser alignment angle	GAMMA	=	unidirectional without fanning
Vertical discharge angle	THETA	=	90 deg
Horizontal discharge angle	SIGMA	=	0 deg
Relative orientation angle	BETA	=	0 deg
Discharge density	RHO0	=	90 deg
Density difference	DRHO	=	1010.5 kg/m <sup>3</sup>
Buoyant acceleration	GPO	=	0 kg/m <sup>3</sup>
Discharge concentration	CO	=	.0000 m/s <sup>2</sup>
Surface heat exchange coeff.	KS	=	5380 CFU-per-100mL
Coefficient of decay	KD	=	0 m/s
		=	0 /s

-----  
FLUX VARIABLES PER UNIT DIFFUSER LENGTH:

Discharge (volume flux)	q0	=	0.000333 m <sup>2</sup> /s
Momentum flux	m0	=	0.000037 m <sup>3</sup> /s <sup>2</sup>
Buoyancy flux	j0	=	0 m <sup>3</sup> /s <sup>3</sup>

-----  
DISCHARGE/ENVIRONMENT LENGTH SCALES :

lq =	0.00 m	lm =	0.00 m	lM =	99999.0 m
------	--------	------	--------	------	-----------

lm' = 99999.0 m lb' = 99999.0 m la = 99999.0 m  
(These refer to the actual discharge/environment length scales.)

-----  
NON-DIMENSIONAL PARAMETERS:

Slot Froude number	FR0	=	99999.0
Port/nozzle Froude number	FRD0	=	99999.0
Velocity ratio	R	=	1.12

-----  
MIXING ZONE / TOXIC DILUTION ZONE / AREA OF INTEREST PARAMETERS:

Toxic discharge		=	yes
CMC concentration	CMC	=	14 CFU-per-100mL
CCC concentration	CCC	=	14 CFU-per-100mL
Water quality standard		=	given by CCC value
Regulatory mixing zone		=	no
Region of interest		=	5000.00 m downstream

\*\*\*\*\*

## HYDRODYNAMIC CLASSIFICATION:

\*-----\*  
| FLOW CLASS = MU2 |  
\*-----\*

This flow configuration applies to a layer corresponding to the full water depth at the discharge site.

Applicable layer depth = water depth = 1.5 m

\*\*\*\*\*

## MIXING ZONE EVALUATION (hydrodynamic and regulatory summary):

-----  
X-Y-Z Coordinate system:

Origin is located at the bottom below the port center:  
250 m from the left bank/shore.

-----  
NEAR-FIELD REGION (NFR) CONDITIONS :

Note: The NFR is the zone of strong initial mixing. It has no regulatory implication. However, this information may be useful for the discharge designer because the mixing in the NFR is usually sensitive to the discharge design conditions.

Pollutant concentration at edge of NFR	=	11.8711 CFU-per-100mL
Dilution at edge of NFR	=	453.2
NFR Location:	x =	150.00 m
(centerline coordinates)	y =	.00 m
	z =	1.50 m
NFR plume dimensions:	half-width =	149.81 m
	thickness =	1.50 m

-----  
Buoyancy assessment:

The effluent density is equal or about equal to the surrounding ambient water density at the discharge level.  
Therefore, the effluent behaves essentially as NEUTRALLY BUOYANT.

-----  
Near-field instability behavior:

The diffuser flow will experience instabilities with full vertical mixing in the near-field.  
There may be benthic impact of high pollutant concentrations.

-----  
FAR-FIELD MIXING SUMMARY:

Plume becomes vertically fully mixed at 150.00 m downstream.

\*\*\*\*\* TOXIC DILUTION ZONE SUMMARY \*\*\*\*\*

Recall: The TDZ corresponds to the three (3) criteria issued in the USEPA Technical Support Document (TSD) for Water Quality-based Toxics Control, 1991 (EPA/505/2-90-001).

Criterion maximum concentration (CMC)	=	14 CFU-per-100mL
---------------------------------------	---	------------------

Corresponding dilution = 384.2  
The CMC was encountered at the following plume position:  
Plume location: x = 24.99 m  
(centerline coordinates) y = .00 m  
z = 1.50 m  
Plume dimensions: half-width = 149.92 m  
thickness = 1.50 m

CRITERION 1: This location is beyond 50 times the discharge length scale of  
 $L_q = 0.159480$  m.

+++++ The discharge length scale TEST for the TDZ has FAILED. +++++

CRITERION 2: This location is beyond 5 times the ambient water depth  
HD = 1.5 m.

+++++ The ambient depth TEST for the TDZ has FAILED. +++++

CRITERION 3: No RMZ has been defined. Therefore, the Regulatory Mixing zone  
test for the TDZ cannot be applied.

The diffuser discharge velocity is equal to 0.11 m/s.

This is less than the minimum of 3.0 m/s recommended in the TSD.

+++ The discharge velocity RECOMMENDATION for the TDZ has NOT been met. +++

\*\*\*\* This discharge DOES NOT SATISFY all three CMC criteria for TDZ. \*\*\*\*

\*\*\*\* This MAY be caused by the low discharge velocity for this design. \*\*\*\*

\*\*\*\*\* REGULATORY MIXING ZONE SUMMARY \*\*\*\*\*

No RMZ has been specified.

However:

The CCC was encountered at the following plume position:

The CCC for the toxic pollutant was encountered at the following

plume position:

CCC = 14 CFU-per-100mL  
Corresponding dilution = 384.2  
Plume location: x = 24.99 m  
(centerline coordinates) y = .00 m  
z = 1.50 m  
Plume dimensions: half-width = 149.92 m  
thickness = 1.50 m

\*\*\*\*\* FINAL DESIGN ADVICE AND COMMENTS \*\*\*\*\*

CORMIX2 uses the TWO-DIMENSIONAL SLOT DIFFUSER CONCEPT to represent  
the actual three-dimensional diffuser geometry. Thus, it approximates  
the details of the merging process of the individual jets from each  
port/nozzle.

In the present design, the spacing between adjacent ports/nozzles  
(or riser assemblies) is somewhat greater (in the range between  
three times to ten times) the local water depth. It is unlikely  
that sufficient lateral interaction of adjacent jets will  
occur in the near-field. However, the individual jets/plumes may merge  
soon after in the intermediate-field or in the far-field.

CORMIX2 may have LIMITED APPLICABILITY for this discharge situation.

The results may be somewhat unrealistic in the near-field (minimum  
dilution may be overpredicted), but appear to be applicable for the  
intermediate- and far-field processes.

The user is advised to use a subsequent CORMIX1 (single port discharge)  
analysis, using discharge data for an individual diffuser jet/plume,  
in order to compare to the present near-field prediction.

-----  
REMINDER: The user must take note that HYDRODYNAMIC MODELING by any known  
technique is NOT AN EXACT SCIENCE.

Extensive comparison with field and laboratory data has shown that the  
CORMIX predictions on dilutions and concentrations (with associated

A-25 (1.5 m)

plume geometries) are reliable for the majority of cases and are accurate to within about  $\pm 50\%$  (standard deviation).

As a further safeguard, CORMIX will not give predictions whenever it judges the design configuration as highly complex and uncertain for prediction.

\*\*\*\*\*

DESIGN CASE: Multiport discharge over one and a half m

FILE NAME: stage2mb

Subsystem CORMIX2: Submerged Multiport Diffuser Discharges

END OF SESSION/ITERATION: 06/30/95--09:04:54

[illegible]

## Appendix B



The Department of Civil Engineering  
College of Engineering and Physical Sciences  
The University of New Hampshire  
Kingsbury Hall  
33 College Road  
Durham, New Hampshire 03824-3591

Project/Problem Set:

Slug Injection

Detail/Problem:

Class: \_\_\_\_\_ Prof: \_\_\_\_\_

Sheet: 31 of 3

Calc. by: Holly Clark

Date: 6/17/95

Chck by: \_\_\_\_\_

Date: \_\_\_\_\_

Given: Mass of slug =  $2 \times 10^9$  CFU  
Velocity = 0.1 m/s  
Channel is 96 m wide  $\times$  3 m deep  $\times$  500 m long

Find: Concentration of fecal coliform using a stream dispersion equation

Theory: McQuivey and Keifer dispersion coefficient equation:

$$D_L = 0.058 \cdot Q / (S_o w) \quad Q = \text{discharge}, S_o = \text{bedslope}, w = \text{stream width}$$

Stream dispersion equation for concentration:

$$C(x, t) = \frac{M}{A(4\pi D_L t)^{1/2}} \exp \left[ -\frac{(x - vt)^2}{4D_L t} \right]$$

Assumptions:  $S_o = 0.001$

Formula is valid for reach not less than 7 stream widths.

① finding discharge,  $Q$

$$Q = VA = (0.1 \text{ m/s})(96 \text{ m} \times 3 \text{ m}) = 28.8 \text{ m}^3/\text{s}$$

② finding dispersion coefficient,  $D_L$

$$D_L = \frac{0.058(28.8)}{(0.001)(96)} = 17.4 \frac{\text{m}^2}{\text{s}}$$

check: at  $t = 3600 \text{ s}$   $x = 360 \text{ m}$  width =  $x/7 = 360/7 = 51$

$$C(360 \text{ m}, 3600 \text{ s}) = \frac{2 \times 10^9 \text{ CFU}}{(10^4 \frac{100 \text{ mL}}{\text{m}^3})(51 \times 3)(4\pi(17.4)(3600))^{1/2}} \exp \left[ -\frac{(360 - 3600(0.1))^2}{4(17.4)(3600)} \right] = 1.4 \frac{\text{CFU}}{100 \text{ mL}}$$

result: The peak concentration of 1.4 CFU/100mL is 360 m downstream one hour after release.

If the slug is fully mixed along the reach:

$$C = \frac{2 \times 10^9 \text{ CFU}}{(96 \times 3)(360 \text{ m})(10^4 \frac{100 \text{ mL}}{\text{m}^3})} = 1.93 \text{ CFU}/100 \text{ mL}$$



The Department of Civil Engineering  
College of Engineering and Physical Sciences  
The University of New Hampshire  
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Project/Problem Set:

Slug Injection

Detail/Problem:

Class:

Prof:

Sheet: R2 of 3

Calc. by: Holly Clark

Date: 6/17/95

Check. by: \_\_\_\_\_

Date: \_\_\_\_\_

③ finding peak concentration at 48 m from slug injection

$$A = 48/7 \times 3 \text{ m} = 20.6 \text{ m}^2$$

$$x = 48 \text{ m}$$

$$v = 0.1 \text{ m/s}$$

$$t = 480 \text{ s}$$

$$x - vt = 0 \therefore \exp \left[ \frac{(x - vt)^2}{4Dt} \right] = 1$$

$$C(48 \text{ m}, 480 \text{ s}) = \frac{2 \times 10^9 \text{ CFU} (10^{-4} \text{ m}^3/100 \text{ mL})}{(20.6 \text{ m}^2)(4\pi(17.4)(480))^{1/2}} = \underline{\underline{30.0 \text{ CFU}/100 \text{ mL}}}$$





Given: Slug injection of  $2 \times 10^9$  CFU =  $C_i V_i$   
Depth of channel is 3 m

Find: Volume of water required to fully mix the slug injection to 14 CFU/100 mL concentration ( $C_f$ ). Find dimensions.

Assume: Ambient water has a 0 CFU/100 mL concentration =  $C_o$

① finding volume required to fully mix to 14 CFU/100 mL concentration,  $V_f$

$$C_i V_i + C_o V_o = C_f V_f$$

$$V_f = \frac{C_i V_i}{C_f} = \frac{2 \times 10^9 \text{ CFU}}{14 \text{ CFU/100 mL}} \left( \frac{1 \times 10^{-4} \text{ m}^3}{100 \text{ mL}} \right) = 14286 \text{ m}^3$$

② finding radius of cylinder

$$\frac{14286 \text{ m}^3}{3 \text{ m}} = 4762 \text{ m}^2$$

$$r = \left[ \frac{4762}{\pi} \right]^{1/2} = 39 \text{ m}$$

If the discharge from the vessel was fully mixed to 14 CFU/100 mL it would spread the full depth of 3 m and reach to a radius of 39 m from the point of injection

If the mud flat is 48 m from the mooring, the fully mixed region would have to move 9 m to hit the mud flat. At 0.1 m/s velocity, it would move 9 m in 90 seconds or 1.5 minutes. Even if it mixes as it moves, this illustrates the extent of mixing that must occur in a relatively short time.

## **APPENDIX III**

### **CORMIX Model and Slug Injection Evaluation Using a Decay Coefficient for Bacterial Die-off**

**Addendum to the  
Diffusion Study on  
Contamination of the Seabrook Clamflat  
in Hampton Harbor**

**Holly C. Gallagher**

**Report Prepared for:**

**Dr. Richard Langan  
June 30, 1995**

Fluids Lab Graduate Office  
Department of Civil Engineering  
Kingsbury Hall  
Durham, NH 03824

June 30, 1995

Dr. Richard Langan  
Jackson Estuarine Laboratory  
Durham, NH 03824

Subject: Addendum to the Diffusion Study on Contamination of the Seabrook Clamflat in Hampton Harbor

Dear Dr. Langan:

The Seabrook area of the Hampton Harbor was re-evaluated incorporating two changes per your suggestion. A decay coefficient of  $10 \text{ day}^{-1}$  was added to the model parameters. A velocity vector that results from a 10 cm/s westerly flow and a 30 cm/s southerly flow was calculated and also added. The CORMIX computer model and an advection-dispersion model were used to evaluate the diffusion of discharges from moored vessels in the channel.

The CORMIX modeling estimated the fecal coliform count to be below 0.018 CFU/100mL as it flowed over the mudflat. A slow release of the contaminant, as modeled by CORMIX, is not a true representation of the intermittent releases expected from the vessels in the harbor. The decay coefficient is time dependent. An small increase in the duration of the discharge is likely to cause a large decrease in the coliform count. Therefore, the predicted value is likely to be exaggerated.

An advection-dispersion model was used to estimate a peak concentration of 13.0 CFU/100mL as the plume reaches the mudflat. The coefficient of longitudinal dispersion used in this model is relatively conservative. Therefore, the concentration of the plume is probably less than the predicted value.

The result of the additional modeling using the decay coefficient and revised flow pattern shows that a vessel release might be sufficiently reduced in concentration within the channel reaches. The revised modeling contradicts the former results. This shows the importance of verification of the assumptions that are used in modeling. The latest results are likely to be more representative of the actual situation. Therefore, it is probable that the clamflats would not be contaminated.

The addendum is included with a copy of the original report. Your consideration of me for this study is appreciated. Please feel free to call at 862-3623 if you have any questions or comments.

Sincerely,

*Holly C. Gallagher*

Holly Clark Gallagher

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## **A1. Introduction:**

### Description of the Revisions

The flow pattern as the tide fills the harbor has been revised. The first modeling assumed that the water filled the channel and then flowed at a velocity of 10cm/s in a westerly direction over the mudflat. The revision includes a combination of a southerly flow at 30cm/s that continues in the channel with the westerly flow of 10cm/s over the mudflat. The resultant flow direction is south-southwest at a velocity of 32cm/s.

A decay coefficient of  $10 \text{ day}^{-1}$  was estimated at Jackson Laboratory. No decay was assumed to occur in the first modeling. The die-off of bacteria in cold seawater is significant and was taken into account in the revised modeling. The decay coefficient is based on disappearance of pathogens due to die-off. It is influenced by the type of bacteria, salinity, temperature, and light intensity. Decay coefficients for fresh water have been measured at 0.12 to  $26 \text{ d}^{-1}$  for coliform. The bacterial decay in seawater is more rapid.

## **A2. Modeling Studies:**

### CORMIX Modeling

The change in flow direction was incorporated in the CORMIX model by adjusting the orientation of the multipoint diffuser. The first stage was run using the 300m (984 ft) long diffuser with 35 ports laid along the centerline of the channel to approximate 35 vessels moored in a similar manner. The initial effluent concentration of 5426700 CFU/100mL was used as before. The only revision was the addition of the decay coefficient to the initial parameters. The discharge from the diffuser is shown to be fully mixed vertically and laterally in the channel in approximately 2 hours. The estimated concentration is 2190 CFU/mL as shown in the CORMIX output (Appendix C). The total CFU discharged by the 35 vessels was reduced using the decay coefficient. The new total that remains after the 2.14 hrs from Stage 1 was used in a mass balance equation to determine the size of the discharge ports for the second stage (Appendix C).

The configuration of the 'river' for Stage 2 matches the flow direction as determined by the revised velocity vector. This results in the multiport diffuser being angled at  $18.4^\circ$ , measured counterclockwise from the ambient flow. The width of the river assumes that the left bank is 48m (157 ft) from the nearest end of the diffuser as it is aligned with the center of the channel. The depth is assumed at 1m (3.3 ft) deep and the width at 500m (1640 ft), which are not changed from the original run. The distance to the mudflat is assumed to be 154m (505 ft) along the 'river' as measured from the center of the diffuser. The decay coefficient was added to the model parameters for the second stage. The result of Stage 2 shows that the effluent plume will be vertically and laterally fully mixed before it reaches the clam beds. The estimated concentration of the plume is 0.0176 CFU/100mL (Appendix C). This is well below the limitation of 14 CFU/100mL.

The CORMIX model simulates a slow release of the effluent over a number of hours. The decay coefficient is time dependent. A small increase in the duration of the contaminant in the seawater causes a large decrease in the concentration. The flow rate in the harbor during flood tide is fast enough to move a discharge from the mooring to the mudflat in approximately 8 minutes. Therefore, the result of the CORMIX model is likely to predict values that are too low.

#### Advection-Dispersion Evaluation of a Slug Injection

An advection-convection model was used to estimate the peak concentration of the plume as it reaches the mudflat. The McQuivey and Keefer method was used to estimate the magnitude of the longitudinal dispersion coefficient at  $55.7 \text{ m}^2/\text{s}$  (Appendix D). This value may be underestimated which would result in a conservative estimate of the plume concentration. The plume is assumed to move in the south-southwesterly direction at 32cm/s. The distance from the mooring to the edge of the mudflat along the flow path is 154m (505 ft). The estimated time elapsed from discharge at the mooring to the mudflat is 8 minutes. The decay coefficient of  $10 \text{ d}^{-1}$  was used in this model. The result of 13 CFU/100mL is below the limitation of 14 CFU/100mL.

### **A3. Conclusion:**

The revised modeling using a decay coefficient and a different flow pattern shows that a vessel release might be considerably reduced in concentration within the channel. The flow direction was changed from west to south-southwest so the plume travels farther before it reaches the mudflat. The decay of the bacteria reduces the coliform count which reduces the concentration. In addition, the plume is more diluted as it moves farther away from the source. Therefore, the die-off of the bacteria and dilution may reduce the coliform count below contamination limits before the plume reaches the clam beds.

The CORMIX results appear to be exaggerated by the long time factor. The slug injection model is conservative and estimates a value below the contamination limit. The accuracy of the advection-dispersion model depends on the determination of the longitudinal dispersion coefficient. The value of the dispersion coefficient could be verified using a tracer study. A laboratory study of the bacteria in a sample of the Hampton Harbor water held at an appropriate temperature could be used to verify the decay coefficient.

The results of the revised modeling are considerably different from the former results. The revision to the advection-dispersion model appears to be a better representation of the actual situation at Hampton Harbor. The vessel discharge into the harbor is likely to be adequately reduced and diluted within the channel to prevent contamination of the mudflats.



## Appendix C

# CORMIX -- CORNELL MIXING ZONE EXPERT SYSTEM -- CORMIX

SITE Name Seabrook Harbor Mudflat Date: 6/28/95  
 Design CASE Multi port discharge w/ decay Prepared by: HC Gallagher  
 DOS FILE NAME STAGE1MD (w/o extension)

**AMBIENT DATA:** Water body is bounded/unbounded  
 Water body depth 3 m If bounded: Width 96 m  
 Depth at discharge 3 m Appearance 1/2/3  
 Ambient flowrate (28) m<sup>3</sup>/s or: Ambient velocity 0.1 m/s  
 Manning's n 0.014 or: Darcy-Weisbach f \_\_\_\_\_  
 Wind speed 2 m/s  
**Density data:** UNITS: Density...kg/m<sup>3</sup> / Temperature...°C  
 Water body is fresh/salt water If fresh: Specify as density/temp. values  
 If uniform: Average density/temp. 1010.5  
 If stratified: Density/temp. at surface \_\_\_\_\_  
 Stratification type A/B/C Density/temp. at bottom \_\_\_\_\_  
 If B/C: Pycnocline height \_\_\_\_\_ m If C: Density/temp. jump \_\_\_\_\_

## DISCHARGE DATA: Specify geometry for CORMIX1 or 2 or 3

### SUBMERGED SINGLE PORT DISCHARGE -- CORMIX1

Nearest bank is on left/right Distance to nearest bank \_\_\_\_\_ m  
 Vertical angle THETA \_\_\_\_\_ ° Horizontal angle SIGMA \_\_\_\_\_ °  
 Port diameter \_\_\_\_\_ m or: Port area \_\_\_\_\_ m<sup>2</sup>  
 Port height \_\_\_\_\_ m

### SUBMERGED MULTIPORT DIFFUSER DISCHARGE -- CORMIX2

Nearest bank is on left/right Distance to one endpoint 48 m  
 Diffuser length 300 m to other endpoint 48 m  
 Total number of openings 35  
 Port diameter 0.051 m with contraction ratio 1  
 Diffuser arrangement/type unidirectional / staged / alternating or vertical B, A  
 Alignment angle GAMMA 0 ° Horizontal angle SIGMA \_\_\_\_\_ °  
 Vertical angle THETA 90 ° Relative orientation BETA \_\_\_\_\_ °  
 Port height 0.99 m A = holes (single ports)

### BUOYANT SURFACE DISCHARGE -- CORMIX3

Discharge located on left/right bank Configuration flush/protruding/co-flowing  
 Horizontal angle SIGMA \_\_\_\_\_ ° If protruding: Dist. fm bank \_\_\_\_\_ m  
 Depth at discharge \_\_\_\_\_ m Bottom slope \_\_\_\_\_ °  
 If rectangular Width \_\_\_\_\_ m or: If circular Diameter \_\_\_\_\_ m  
 discharge channel: Depth \_\_\_\_\_ m pipe: Bottom invert depth \_\_\_\_\_ m

Effluent: Flow rate 0.00714 m<sup>3</sup>/s or: Effluent velocity \_\_\_\_\_ m/s  
 Effluent density 1010.15 kg/m<sup>3</sup> or: Effluent temperature \_\_\_\_\_ °C  
 Heated discharge? yes/no If yes: Heat loss coefficient \_\_\_\_\_ W/m<sup>2</sup>, °C  
 Concentration units CFU-PER-100mL Effluent concentration 5426700  
 Conservative substance? yes/no If no: Decay coefficient 10 /day

### MIXING ZONE DATA:

Is effluent toxic? yes/no If yes: CMC value 14  
 CCC value 14  
 WQ stand./conventional poll.? yes/no If yes: value of standard \_\_\_\_\_  
 Any mixing zone specified? yes/no If yes: distance \_\_\_\_\_ m  
 or width \_\_\_\_\_ % or m  
 or area \_\_\_\_\_ % or m<sup>2</sup>  
 Region of interest 1000 m  
 Grid intervals for display 6

## CORMIX2 PREDICTION FILE:

[illegible]

## CORNELL MIXING ZONE EXPERT SYSTEM

Subsystem CORMIX2:

Subsystem version:

Submerged Multiport Diffuser Discharges CMX2 v.2.10

May 1993

### CASE DESCRIPTION

```
Site name/label:      Seabrook^Harbor^Mudflat
Design case:          Multiport^discharge^with^decay
FILE NAME:            cormix\sim\stagelmd.cx2
Time of Fortran run:  06/29/95--08:48:47
```

## ENVIRONMENT PARAMETERS (metric units)

```

Bounded section
BS      =      96.00  AS      =      288.00  QA      =      28.80
HA      =       3.00  HD      =       3.00
UA      =       .100  F        =       .011  USTAR = .3651E-02
UW      =       2.000  UWSTAR= .2198E-02
Uniform density environment
STRCND=  U          RHOAM = 1010.5000

```

### DIFFUSER DISCHARGE PARAMETERS (metric units)

```

DITYPE=alternating parallel
BETYPE=alternating without fanning
BANK  =  LEFT      DISTB =      .00  YB1  =      48.00  YB2  =      48.00
LD    =      300.00  NOPEN =      35      SPAC  =      8.82
DO    =      .051  AO    =      .002  HO    =      .99
GAMMA =      .00  THETA =      90.00
SIGMA =      .00  BETA  =      90.00
UO    =      .100  QO    =      .007      = .7140E-02
RHO0  = 1010.1500  DRHO0 = .3500E+00  GP0   = .3396E-02
CO    = .5427E+07  CUNITS= CFU-per-100mL
IPOLL = 2          KS    = .0000E+00  KD    = .1160E-03

```

DIFFUSER PARAMETERS WITH IMAGE EFFECTS (metric units)

The bank/shore proximity effect is accounted for by the following flow variables and definitions of length scales and parameters.

LD = 300.00 00 = .014 (00 = .1428E-01)

FLUX VARIABLES - PER UNIT DIFFUSER LENGTH (metric units)

```

q0      = .9500E-04  m0      = .2370E-05  j0      = .8067E-07  SIGNJ0=      1.0
Associated 2-d length scales (meters)
lQ=B    =      .001  lM      =      .13    lm      =      .00
lmp     = 99999.00  lbp     = 99999.00  la      = 99999.00

```

FLUX VARIABLES - ENTIRE DIFFUSER (metric units)

Q0	= .1428E-01	M0	= .7111E-03	J0	= .2420E-04				
Associated 3-d length scales (meters)									
LQ	= .41	LM	= .89	Lm	= .35	Lb	= .05		
				Lmp	= 99999.00	Lbp	= 99999.00		

## NON-DIMENSIONAL PARAMETERS

FR0	=	110.99	FRD0	=	7.58	R	=	.99
(slot)			(port/nozzle)					

## FLOW CLASSIFICATION

[illegible]



END OF MOD222: STRONGLY DEFLECTED PLANE PLUME IN CROSSFLOW

---

BEGIN MOD243: DENSITY CURRENT DEVELOPING ALONG PARALLEL DIFFUSER LINE

The plume for this parallel diffuser interacts with the surface/pycnocline or the bottom, and a DENSITY CURRENT forms.

Note: The starting x-coordinate of the developing plume will be shifted upstream.

Profile definitions:

BV = top-hat thickness, measured vertically

BH = top-hat half-width, measured horizontally in y-direction

ZU = upper plume boundary (Z-coordinate)

ZL = lower plume boundary (Z-coordinate)

S = hydrodynamic average (bulk) dilution

C = average (bulk) concentration (includes reaction effects, if any)

X	Y	Z	S	C	BV	BH
323.04	.00	3.00	2834.8	.111E+04	.90	.90
373.04	.00	3.00	4009.0	.738E+03	3.00	.95
423.04	.00	3.00	4009.0	.696E+03	3.00	.99
473.04	.00	3.00	4009.0	.657E+03	3.00	1.04
523.04	.00	3.00	4009.0	.620E+03	3.00	1.09
573.04	.00	3.00	4009.0	.585E+03	3.00	1.14
623.04	.00	3.00	4009.0	.552E+03	3.00	1.19

Cumulative travel time = 7730. sec

END OF MOD243: DENSITY CURRENT DEVELOPING ALONG PARALLEL DIFFUSER LINE

---

\*\* End of NEAR-FIELD REGION (NFR) \*\*

Recall that the plume is symmetric to the bank/shore on which the centerline (X-axis) is located.

The LIMITING DILUTION (given by ambient flow/discharge ratio) is: 1009.4

This value is below the computed dilution of 4009.0 at the end of the NFR.

Mixing for this discharge configuration is constrained by the ambient flow.

The previous module predictions are unreliable since the limiting dilution cannot be exceeded for this diffuser in deep unstratified layer.

A subsequent module (MOD281) will predict the properties of the cross-sectionally fully mixed plume with limiting dilution and will compute a POSSIBLE UPSTREAM WEDGE INTRUSION.

---

BEGIN MOD281: MIXED PLUME/BOUNDED CHANNEL/POSSIBLE UPSTREAM WEDGE INTRUSION

The DOWNSTREAM flow field for this unstable shallow water discharge is VERTICALLY FULLY MIXED.

The mixing is controlled by the limiting dilution = 1009.4

Channel DENSIMETRIC FROUDE NUMBER (FCHAN) for this mixed flow = 31.47

No upstream wedge intrusion takes place since FCHAN exceeds the critical value of 0.7.

X	Y	Z	S	C	BV	BH	ZU	ZL
623.04	.00	3.00	1009.4	.219E+04	3.00	96.00	3.00	.00

Cumulative travel time = 7730. sec



## CORMIX SESSION REPORT:

XX

## CORMIX: CORNELL MIXING ZONE EXPERT SYSTEM

CORMIX v.2.10

May 1993

SITE NAME/LABEL: Seabrook Harbor Mudflat  
 DESIGN CASE: Multiport discharge with decay  
 FILE NAME: stage1md  
 Using subsystem CORMIX2: Submerged Multiport Diffuser Discharges  
 Start of session: 06/29/95--08:43:27

\*\*\*\*\*

## SUMMARY OF INPUT DATA:

-----  
AMBIENT PARAMETERS:

Cross-section		=	bounded
Width	BS	=	96 m
Channel regularity		=	1
Ambient flowrate	QA	=	28.80 m <sup>3</sup> /s
Average depth	HA	=	3 m
Depth at discharge	HD	=	3 m
Ambient velocity	UA	=	.1 m/s
Darcy-Weisbach friction factor	F	=	0.0106
Calculated from Manning's n		=	.014
Wind velocity	UW	=	2 m/s
Stratification Type	STRCND	=	U
Surface density	RHOAS	=	1010.5 kg/m <sup>3</sup>
Bottom density	RHOAB	=	1010.5 kg/m <sup>3</sup>

-----  
DISCHARGE PARAMETERS:

## Submerged Multiport Diffuser Discharge

Diffuser type	DITYPE	=	alternating parallel
Diffuser length	LD	=	300 m
Nearest bank		=	left
Diffuser endpoints	YB1	=	48 m; YB2 = 48 m
Number of openings	NOPEN	=	35
Spacing between risers/openings	SPAC	=	8.82 m
Port/Nozzle diameter	D0	=	.051 m
Equivalent slot width	B0	=	0.0002 m
Total area of openings	A0	=	0.0020 m <sup>2</sup>
Discharge velocity	U0	=	0.09 m/s
Total discharge	Q0	=	.00714 m <sup>3</sup> /s
Discharge port height	H0	=	.99 m
Nozzle arrangement	BETYPE	=	alternating without fanning
Diffuser alignment angle	GAMMA	=	0 deg
Vertical discharge angle	THETA	=	90.0 deg
Horizontal discharge angle	SIGMA	=	0.0 deg
Relative orientation angle	BETA	=	90.0 deg
Discharge density	RHO0	=	1010.15 kg/m <sup>3</sup>
Density difference	DRHO	=	0.3500 kg/m <sup>3</sup>
Buoyant acceleration	GP0	=	.0034 m/s <sup>2</sup>
Discharge concentration	C0	=	5426700 CFU-per-100mL
Surface heat exchange coeff.	KS	=	0 m/s
Coefficient of decay	KD	=	0.000116 /s

-----  
FLUX VARIABLES PER UNIT DIFFUSER LENGTH:

Discharge (volume flux)	q0	=	0.000095 m <sup>2</sup> /s
Momentum flux	m0	=	0.000004 m <sup>3</sup> /s <sup>2</sup>
Buoyancy flux	j0	=	0 m <sup>3</sup> /s <sup>3</sup>

-----  
DISCHARGE/ENVIRONMENT LENGTH SCALES :

lq =	0.00 m	lm =	0.00 m	lM =	0.12 m
------	--------	------	--------	------	--------

lm' = 99999.0 m      lb' = 99999.0 m      la = 99999.0 m  
 (These refer to the actual discharge/environment length scales.)

#### NON-DIMENSIONAL PARAMETERS:

Slot Froude number	FRO	=	110.99
Port/nozzle Froude number	FRDO	=	7.58
Velocity ratio	R	=	0.99

#### MIXING ZONE / TOXIC DILUTION ZONE / AREA OF INTEREST PARAMETERS:

Toxic discharge		=	yes
CMC concentration	CMC	=	14 CFU-per-100mL
CCC concentration	CCC	=	14 CFU-per-100mL
Water quality standard		=	given by CCC value
Regulatory mixing zone		=	no
Region of interest		=	1000.00 m downstream

\*\*\*\*\*

#### HYDRODYNAMIC CLASSIFICATION:

\*-----\*  
 | FLOW CLASS = MU1H |  
 \*-----\*

This flow configuration applies to a layer corresponding to the full water depth at the discharge site.

Applicable layer depth = water depth = 3 m

\*\*\*\*\*

#### MIXING ZONE EVALUATION (hydrodynamic and regulatory summary):

#### X-Y-Z Coordinate system:

Origin is located at the bottom below the port center:  
 0.0 m from the left bank/shore.

#### NEAR-FIELD REGION (NFR) CONDITIONS :

Note: The NFR is the zone of strong initial mixing. It has no regulatory implication. However, this information may be useful for the discharge designer because the mixing in the NFR is usually sensitive to the discharge design conditions.

Pollutant concentration at edge of NFR	=	552.1489 CFU-per-100mL
Dilution at edge of NFR	=	4008.9
NFR Location:	x =	623.04 m
(centerline coordinates)	y =	.00 m
	z =	3.00 m
NFR plume dimensions:	half-width =	1.18 m
	thickness =	3.00 m

#### Buoyancy assessment:

The effluent density is less than the surrounding ambient water density at the discharge level.

Therefore, the effluent is POSITIVELY BUOYANT and will tend to rise towards the surface.

#### \*\*\*\*\* TOXIC DILUTION ZONE SUMMARY \*\*\*\*\*

Criterion maximum concentration (CMC)	=	14 CFU-per-100mL
Corresponding dilution	=	.0

The CMC value was not encountered within the specified simulation distance.

Plume dilution values are too low to meet CMC.

#### \*\*\*\*\* REGULATORY MIXING ZONE SUMMARY \*\*\*\*\*

No RMZ has been specified.

The CCC for the toxic pollutant was not encountered within the predicted plume region.

#### \*\*\*\*\* FINAL DESIGN ADVICE AND COMMENTS \*\*\*\*\*

CORMIX2 uses the TWO-DIMENSIONAL SLOT DIFFUSER CONCEPT to represent







Given:  $2 \times 10^9$  CFU per vessel

35 vessels

Initial concentration = 2190 CFU/100 mL

Decay coeff =  $10 \text{ d}^{-1} = 0.000116 \text{ s}^{-1}$

Velocity components are 0.1 m/s toward mudflat from centerline of channel and 0.3 m/s along centerline of channel

Find: Port diameter for 35 equal sized ports if discharge is continuous for 4 hrs

① finding total CFU after 7730 sec (from stage 1)

$$M = (2 \times 10^9 \text{ CFU})(35) \exp[(-0.000116 \text{ s}^{-1})(7730 \text{ sec})] = 2.86 \times 10^{10}$$

② finding volume,  $V$

$$V = \frac{2.86 \times 10^{10}}{2190 \text{ CFU/100 mL}} (1 \times 10^{-6} \text{ m}^3/\text{mL}) = 1304 \text{ m}^3$$

③ finding total discharge,  $Q$

$$Q = 1304 \text{ m}^3 / 4 \text{ hr} (3600 \text{ s/hr}) = 0.0906 \text{ m}^3/\text{s}$$

④ finding magnitude of velocity

$$V = (0.1^2 + 0.3^2)^{1/2} = 0.32 \text{ m/s}$$

⑤ finding area of Port,  $A$

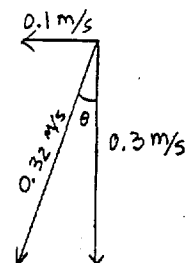
$$A = \frac{Q}{V} = \frac{0.0906 \text{ m}^3/\text{s}}{(0.32 \text{ m/s})(35)} = 0.0081 \text{ m}^2/\text{port}$$

⑥ finding diameter of Port,  $d$

$$d = \sqrt{\frac{4A}{\pi}} = 0.101 \text{ m}$$

⑦ finding angle of flow to diffuser,  $\theta$

$$\theta = \tan^{-1}(0.1/0.3) = 18.4^\circ$$



# CORMIX -- CORNELL MIXING ZONE EXPERT SYSTEM -- CORMIX

SITE Name Seabrook Harbor Mudflat Date: 6/28/95  
 Design CASE Multiport discharge w/ decan Prepared by: H.C. Gallagher  
 DOS FILE NAME Stage 2D (w/o extension)

**AMBIENT DATA:** Water body is bounded/unbounded  
 Water body depth 1 m If bounded: Width 500 m  
 Depth at discharge 1 m Appearance 1/2/3  
 Ambient flowrate        m<sup>3</sup>/s or: Ambient velocity 0.32 m/s  
 Manning's n 0.014 or: Darcy-Weisbach f         
 Wind speed 2 m/s  
**Density data:** UNITS: Density...kg/m<sup>3</sup> / Temperature...°C  
 Water body is fresh/salt water If fresh: Specify as density/temp. values  
 If uniform: Average density/temp. 1010.5  
 If stratified: Density/temp. at surface         
 Stratification type A/B/C Density/temp. at bottom         
 If B/C: Pycnocline height        m If C: Density/temp. jump       

**DISCHARGE DATA:** Specify geometry for CORMIX1 or 2 or 3

## SUBMERGED SINGLE PORT DISCHARGE -- CORMIX1

Nearest bank is on left/right Distance to nearest bank        m  
 Vertical angle THETA        ° Horizontal angle SIGMA        °  
 Port diameter        m or: Port area        m<sup>2</sup>  
 Port height        m

## SUBMERGED MULTIPOINT DIFFUSER DISCHARGE -- CORMIX2

Nearest bank is on left/right Distance to one endpoint 143 m  
 Diffuser length 300 m to other endpoint 48 m  
 Total number of openings 35  
 Port diameter 0.101 m with contraction ratio 1  
 Diffuser arrangement/type unidirectional / staged / alternating or vertical  
 Alignment angle GAMMA 18.4 ° Horizontal angle SIGMA 0 co-flowing °  
 Vertical angle THETA 0 horiz Relative orientation BETA 18.4 °  
 Port height 0.33 m

## BUOYANT SURFACE DISCHARGE -- CORMIX3

Discharge located on left/right bank Configuration flush/protruding/co-flowing  
 Horizontal angle SIGMA        ° If protruding: Dist. frm bank        m  
 Depth at discharge        m Bottom slope        °  
 If rectangular Width        m or: If circular Diameter        m  
discharge channel: Depth        m pipe: Bottom invert depth        m

**Effluent:** Flow rate 0.0906 m<sup>3</sup>/s or: Effluent velocity        m/s  
 Effluent density 1010.5 kg/m<sup>3</sup> or: Effluent temperature        °C  
 Heated discharge? yes/no If yes: Heat loss coefficient        W/m<sup>2</sup>, °C  
 Concentration units cpu per 100ml Effluent concentration 2190  
 Conservative substance? yes/no If no: Decay coefficient 10 /day

## MIXING ZONE DATA:

Is effluent toxic? yes/no If yes: CMC value 14  
 CCC value 14  
 WQ stand./conventional poll.? yes/no If yes: value of standard         
 Any mixing zone specified? yes/no If yes: distance        m  
 or width        % or m  
 or area        % or m<sup>2</sup>  
 Region of interest 5000 m  
 Grid intervals for display 6





standard or CCC value.

-7.28	.00	1.00	2.8	.374E+01	1.00	42.72
37.74	.00	1.00	2.8	.627E+00	1.00	56.96
82.76	.00	1.00	2.8	.105E+00	1.00	71.20
127.78	.00	1.00	2.8	.176E-01	1.00	85.44
Cumulative travel time =			92384. sec			

END OF MOD274: ACCELERATION ZONE OF STAGED DIFFUSER

BEGIN MOD251: DIFFUSER PLUME IN CO-FLOW

Phase 1: Vertically mixed, Phase 2: Re-stratified

This flow region is INSIGNIFICANT in spatial extent and will be by-passed.

END OF MOD251: DIFFUSER PLUME IN CO-FLOW

\*\* End of NEAR-FIELD REGION (NFR) \*\*

The initial plume WIDTH values in the next far-field module will be  
CORRECTED by a factor .10 to conserve the mass flux in the far-field!

Recall that the plume is symmetric to the bank/shore on which the centerline  
(X-axis) is located.

BEGIN MOD241: BUOYANT AMBIENT SPREADING

Plume is ATTACHED to LEFT bank/shore.

Plume width is now determined from LEFT bank/shore.

Discharge is non-buoyant or weakly buoyant.  
Therefore BUOYANT SPREADING REGIME is ABSENT.

END OF MOD241: BUOYANT AMBIENT SPREADING

BEGIN MOD261: PASSIVE AMBIENT MIXING IN UNIFORM AMBIENT

Vertical diffusivity (initial value) = .281E-02 m<sup>2</sup>/s  
Horizontal diffusivity (initial value) = .351E-02 m<sup>2</sup>/s

The passive diffusion plume is VERTICALLY FULLY MIXED at beginning of region.

Profile definitions:

BV = Gaussian s.d.\*sqrt(pi/2) (46%) thickness, measured vertically  
= or equal to layer depth, if fully mixed

BH = Gaussian s.d.\*sqrt(pi/2) (46%) half-width,  
measured horizontally in Y-direction

ZU = upper plume boundary (Z-coordinate)

ZL = lower plume boundary (Z-coordinate)

S = hydrodynamic centerline dilution

C = centerline concentration (includes reaction effects, if any)

Plume Stage 2 (bank attached):

X	Y	Z	S	C	BV	BH	ZU	ZL
127.78	.00	1.00	2.8	.176E-01	1.00	1.56	1.00	.00
939.82	.00	1.00	9.7	.371E-02	1.00	5.52	1.00	.00
1751.85	.00	1.00	13.5	.200E-02	1.00	7.65	1.00	.00
2563.89	.00	1.00	16.4	.122E-02	1.00	9.30	1.00	.00

END OF MOD261: PASSIVE AMBIENT MIXING IN UNIFORM AMBIENT

A SUBSEQUENT APPLICATION OF CORMIX1 IS RECOMMENDED to provide more detail for one of the individual jets/plumes in the initial region before merging.

[illegible]

## CORMIX SESSION REPORT:

XX

CORMIX: CORNELL MIXING ZONE EXPERT SYSTEM

CORMIX v.2.10

May 1993

SITE NAME/LABEL:

Seabrook Harbor Mudflat

DESIGN CASE:

Multiport discharge with decay

FILE NAME:

stage2d

Using subsystem CORMIX2:

Submerged Multiport Diffuser Discharges

Start of session:

06/29/95--14:40:12

\*\*\*\*\*

## SUMMARY OF INPUT DATA:

-----  
AMBIENT PARAMETERS:

Cross-section		=	bounded
Width	BS	=	500 m
Channel regularity		=	1
Ambient flowrate	QA	=	160 m <sup>3</sup> /s
Average depth	HA	=	1 m
Depth at discharge	HD	=	1 m
Ambient velocity	UA	=	.32 m/s
Darcy-Weisbach friction factor	F	=	0.0153
Calculated from Manning's n		=	0.014
Wind velocity	UW	=	2 m/s
Stratification Type	STRCND	=	U
Surface density	RHOAS	=	1010.5 kg/m <sup>3</sup>
Bottom density	RHOAB	=	1010.5 kg/m <sup>3</sup>

-----  
DISCHARGE PARAMETERS:

	Submerged Multiport Diffuser Discharge		
Diffuser type	DITYPE	=	staged parallel
Diffuser length	LD	=	300 m
Nearest bank		=	left
Diffuser endpoints	YB1	=	48 m; YB2 = 143 m
Number of openings	NOPEN	=	35
Spacing between risers/openings	SPAC	=	8.82 m
Port/Nozzle diameter	D0	=	.101 m
Equivalent slot width	B0	=	0.0009 m
Total area of openings	A0	=	0.0080 m <sup>2</sup>
Discharge velocity	U0	=	0.32 m/s
Total discharge	Q0	=	.0906 m <sup>3</sup> /s
Discharge port height	H0	=	.33 m
Nozzle arrangement	BETYPE	=	staged
Diffuser alignment angle	GAMMA	=	18.4 deg
Vertical discharge angle	THETA	=	0 deg
Horizontal discharge angle	SIGMA	=	0 deg
Relative orientation angle	BETA	=	18.4 deg
Discharge density	RHO0	=	1010.5 kg/m <sup>3</sup>
Density difference	DRHO	=	0 kg/m <sup>3</sup>
Buoyant acceleration	GPO	=	.0000 m/s <sup>2</sup>
Discharge concentration	C0	=	2190 CFU-per-100mL
Surface heat exchange coeff.	KS	=	0 m/s
Coefficient of decay	KD	=	0.000116 /s

-----  
FLUX VARIABLES PER UNIT DIFFUSER LENGTH:

Discharge (volume flux)	q0	=	0.001342 m <sup>2</sup> /s
Momentum flux	m0	=	0.000207 m <sup>3</sup> /s <sup>2</sup>
Buoyancy flux	j0	=	0 m <sup>3</sup> /s <sup>3</sup>

-----  
DISCHARGE/ENVIRONMENT LENGTH SCALES :

lq =	0.00 m	lm =	0.00 m	lM =	99999.0 m
------	--------	------	--------	------	-----------



lm' = 99999.0 m      lb' = 99999.0 m      la = 99999.0 m  
(These refer to the actual discharge/environment length scales.)

#### NON-DIMENSIONAL PARAMETERS:

Slot Froude number	FR0	=	99999.0
Port/nozzle Froude number	FRD0	=	99999.0
Velocity ratio	R	=	1.00

#### MIXING ZONE / TOXIC DILUTION ZONE / AREA OF INTEREST PARAMETERS:

Toxic discharge		=	yes
CMC concentration	CMC	=	14 CFU-per-100mL
CCC concentration	CCC	=	14 CFU-per-100mL
Water quality standard		=	given by CCC value
Regulatory mixing zone		=	no
Region of interest		=	5000.00 m downstream

\*\*\*\*\*

#### HYDRODYNAMIC CLASSIFICATION:

\*-----\*

FLOW CLASS	=	MU7	
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\*-----\*

This flow configuration applies to a layer corresponding to the full water depth at the discharge site.

Applicable layer depth = water depth = 1 m

\*\*\*\*\*

#### MIXING ZONE EVALUATION (hydrodynamic and regulatory summary):

#### X-Y-Z Coordinate system:

Origin is located at the bottom below the port center:  
0.0 m from the left bank/shore.

#### NEAR-FIELD REGION (NFR) CONDITIONS :

Note: The NFR is the zone of strong initial mixing. It has no regulatory implication. However, this information may be useful for the discharge designer because the mixing in the NFR is usually sensitive to the discharge design conditions.

Pollutant concentration at edge of NFR	=	.0176 CFU-per-100mL
Dilution at edge of NFR	=	2.7
NFR Location:	x =	127.78 m
(centerline coordinates)	y =	.00 m
	z =	1.00 m
NFR plume dimensions:	half-width =	85.44 m
	thickness =	1.00 m

#### Buoyancy assessment:

The effluent density is equal or about equal to the surrounding ambient water density at the discharge level.

Therefore, the effluent behaves essentially as NEUTRALLY BUOYANT.

#### Near-field instability behavior:

The diffuser flow will experience instabilities with full vertical mixing in the near-field.

There may be benthic impact of high pollutant concentrations.

#### FAR-FIELD MIXING SUMMARY:

Plume becomes vertically fully mixed at 127.78 m downstream.

\*\*\*\*\* TOXIC DILUTION ZONE SUMMARY \*\*\*\*\*

Recall: The TDZ corresponds to the three (3) criteria issued in the USEPA Technical Support Document (TSD) for Water Quality-based Toxics Control, 1991 (EPA/505/2-90-001).

Criterion maximum concentration (CMC)	=	14 CFU-per-100mL
---------------------------------------	---	------------------

Corresponding dilution = 156.4  
 The CMC was encountered at the following plume position:  
 Plume location: x = -32.14 m  
                   (centerline coordinates) y = .00 m  
   z = 1.00 m  
 Plume dimensions: half-width = 34.85 m  
   thickness = 1.00 m  
 CRITERION 1: This location is within 50 times the discharge length scale of  
                    $L_q = 0.089486$  m.  
 +++++ The discharge length scale TEST for the TDZ has been SATISFIED. +++++  
 CRITERION 2: This location is within 5 times the ambient water depth  
                   HD = 1 m.  
 ++++++ The ambient depth TEST for the TDZ has been SATISFIED.+++++  
 CRITERION 3: No RMZ has been defined. Therefore, the Regulatory Mixing zone  
                   test for the TDZ cannot be applied.  
 The diffuser discharge velocity is equal to 0.32 m/s.  
 This is less than the minimum of 3.0 m/s recommended in the TSD.  
 +++ The discharge velocity RECOMMENDATION for the TDZ has NOT been met. +++

\*\*\* All three CMC criteria for the TDZ are SATISFIED for this discharge. \*\*\*  
 \*\*\*\*\* REGULATORY MIXING ZONE SUMMARY \*\*\*\*\*  
 No RMZ has been specified.

However:

The CCC was encountered at the following plume position:  
 The CCC for the toxic pollutant was encountered at the following  
 plume position:

CCC = 14 CFU-per-100mL  
 Corresponding dilution = 156.4  
 Plume location: x = -32.14 m  
                   (centerline coordinates) y = .00 m  
   z = 1.00 m  
 Plume dimensions: half-width = 34.85 m  
   thickness = 1.00 m

\*\*\*\*\* FINAL DESIGN ADVICE AND COMMENTS \*\*\*\*\*  
 CORMIX2 uses the TWO-DIMENSIONAL SLOT DIFFUSER CONCEPT to represent  
 the actual three-dimensional diffuser geometry. Thus, it approximates  
 the details of the merging process of the individual jets from each  
 port/nozzle.

In the present design, the spacing between adjacent ports/nozzles  
 (or riser assemblies) is somewhat greater (in the range between  
 three times to ten times) the local water depth. It is unlikely  
 that sufficient lateral interaction of adjacent jets will  
 occur in the near-field. However, the individual jets/plumes may merge  
 soon after in the intermediate-field or in the far-field.

CORMIX2 may have LIMITED APPLICABILITY for this discharge situation.

The results may be somewhat unrealistic in the near-field (minimum  
 dilution may be overpredicted), but appear to be applicable for the  
 intermediate- and far-field processes.

The user is advised to use a subsequent CORMIX1 (single port discharge)  
 analysis, using discharge data for an individual diffuser jet/plume,  
 in order to compare to the present near-field prediction.

-----  
 This parallel diffuser lies in CLOSE PROXIMITY to the bank (shoreline). The  
 shoreline will act as a REFLECTING BOUNDARY for the flow field. This effect  
 has been represented by doubling all flow variables.  
 -----

REMINDER: The user must take note that HYDRODYNAMIC MODELING by any known

As a further safeguard, CORMIX will not give predictions whenever it judges the design configuration as highly complex and uncertain for prediction.

\*\*\*\*\*

```
DESIGN CASE: Multiport discharge with decay
FILE NAME: stage2d
Subsystem CORMIX2: Submerged Multiport Diffuser Discharges
END OF SESSION/ITERATION: 06/30/95--09:12:02
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[illegible]

## Appendix D



The Department of Civil Engineering  
College of Engineering and Physical Sciences  
The University of New Hampshire  
Kingsbury Hall  
33 College Road  
Durham, New Hampshire 03824-3591

Project/Problem Set:

Slug Injection

Detail/Problem:

with Decay Coefficient

Class:

Prof:

Sheet: D-1 of 1

Calc. by: H.C. Gallagher

Date: 6/28/95

Chck. by:

Date:

Given: Mass of Slug =  $2 \times 10^9$  CFU

Velocity = 0.3 m/s along channel and 0.1 m/s across channel

Channel is 101.2 m wide  $\times$  3 m deep  $\times$  500 m Long (normal to flow)

Decay coefficient =  $K = 10 \text{ d}^{-1}$

Find: Concentration of fecal coliform using a stream dispersion equation

Theory: McQuivey and Keeter dispersion coefficient equation

$$D_L = 0.058 \frac{Q}{(S_o W)} = 0.058 \frac{v A}{S_o W} = 0.058 \frac{v d}{S_o}$$

Stream dispersion equation for concentration

$$c(x, t) = \frac{M \exp[-Kt]}{A (4\pi D_L t)^{1/2}} \exp\left[-\frac{(x-vt)^2}{4D_L t}\right] \quad (\text{Metcalfe & Eddy, 1972 p1214})$$

Assumptions:  $S_o = 0.001$

Decay coefficient is applied to reduce concentration prior to calculating final concentration

Formula is valid for reach not less than 7 stream widths.

① finding magnitude of net velocity,  $v$

$$v = (0.1^2 + 0.3^2)^{1/2} = 0.32 \text{ m/s}$$

② finding  $D_L$

$$D_L = 0.058 (0.32)(3)/0.001 = 55.7 \text{ m}^2/\text{s}$$

③ finding distance to clamat along velocity vector

$$x = (48 \text{ m})(0.32 \text{ m/s})/(0.1 \text{ m/s}) = 154 \text{ m}$$

④ finding peak concentration at  $x = 154 \text{ m}$  from slug injection

$$A = \frac{154}{7} \times 3 = 25 \text{ m}^2$$

$$v = 0.32 \text{ m/s}$$

$$t = 481 \text{ s}$$

$$x - vt = 0 \therefore \exp\left[-\frac{(x-vt)^2}{4D_L t}\right] = 1$$

$$c(154 \text{ m}, 481 \text{ s}) = \frac{(2 \times 10^9 \text{ CFU})(10^{-4} \frac{\text{m}^3}{100 \text{ mL}})(\exp[-10 \text{ d}^{-1}(481 \text{ s})(1.157 \times 10^{-5} \text{ d/s})])}{(25 \text{ m}^2)(4\pi(55.7 \text{ m}^2/\text{s})(481 \text{ s}))^{1/2}} = 13.0 \frac{\text{CFU}}{100 \text{ mL}}$$